



UiO : Department of Chemistry
University of Oslo



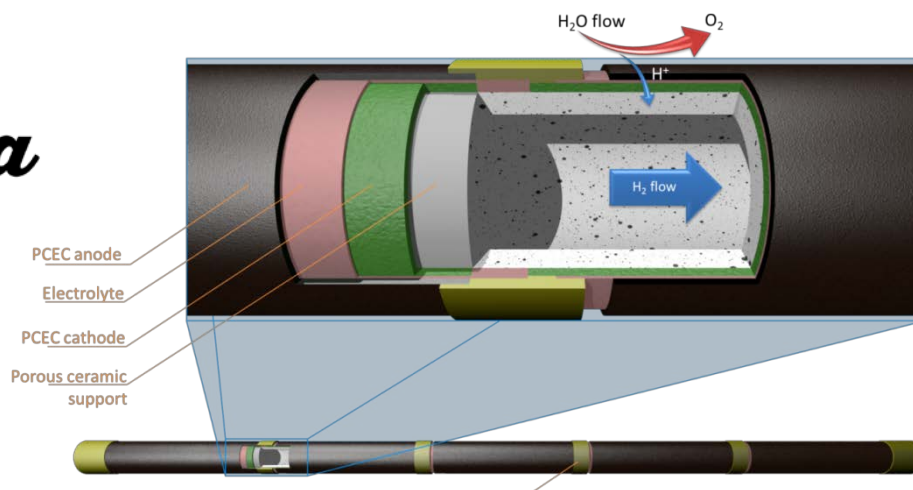
Development of Tubular Proton Ceramic Electrolysers (PCEs)

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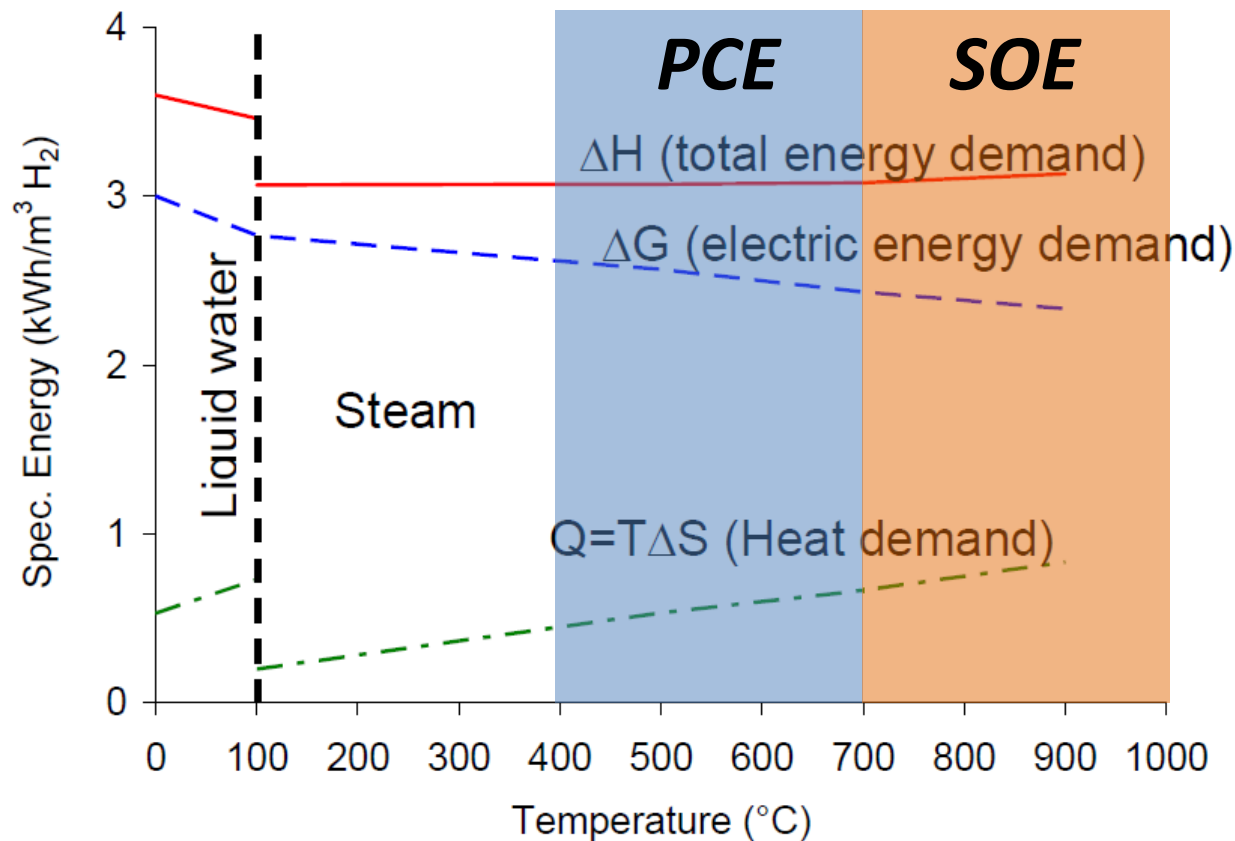
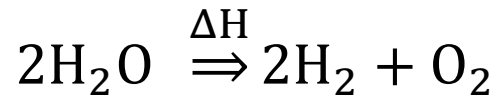


Electra



- Why PCE?
- Processing & performance
- Up-scaling of tubular PCEs

High temperature electrolysis enables utilization of waste heat resources

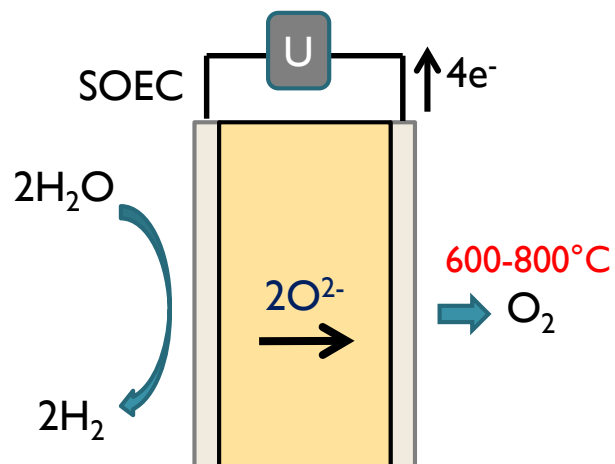


Key differences between SOE and PCE

- advantages and challenges

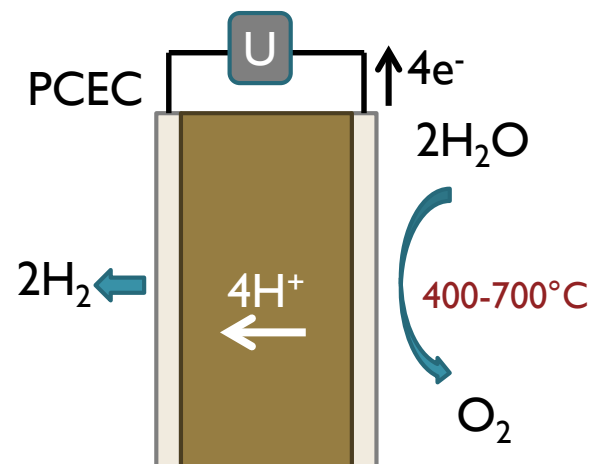
▶ Solid Oxide Electrolysers

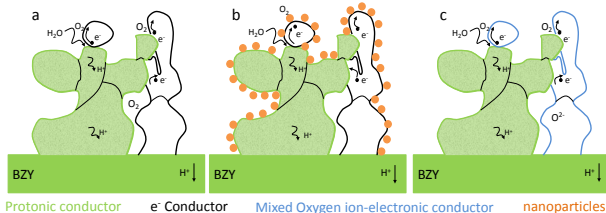
- ▶ Well proven technology
 - ▶ Scalable production
 - ▶ High current densities at thermo-neutral voltage
- ▶ Long term stability challenges
 - ▶ Delamination of O₂-electrode
 - ▶ Oxidation and degradation of Ni-electrode with high steam contents and/or low currents
- ▶ High temperatures



▶ Proton Ceramic Electrolysers

- ▶ Less mature technology
 - ▶ Fabrication and processing challenges
- ▶ Produces dry H₂ directly
- ▶ Potentially intermediate temperatures
 - ▶ Slow O₂-electrode kinetics





Development of tubular cathode supported electrolyte cell

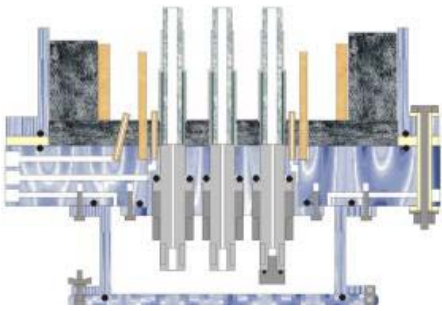


Development and optimization of anodes and current collection

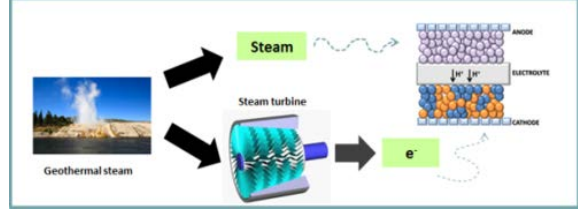
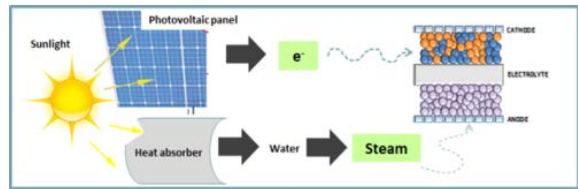
Single tube module development and testing



Multi-tube module testing
Aim: 1kW demo



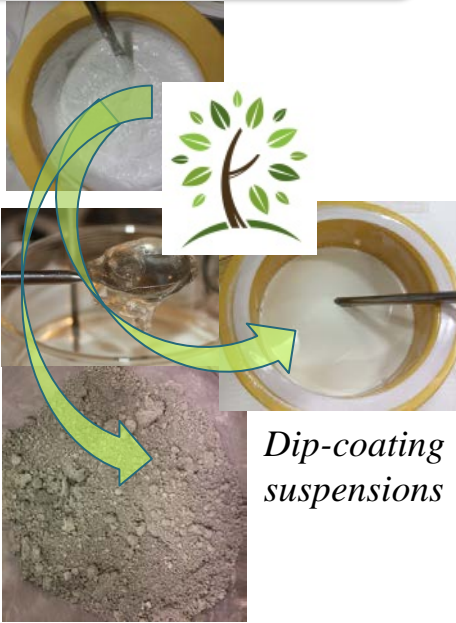
Process integration and evaluation





Tubular half-cell production

Wet milling of precursors



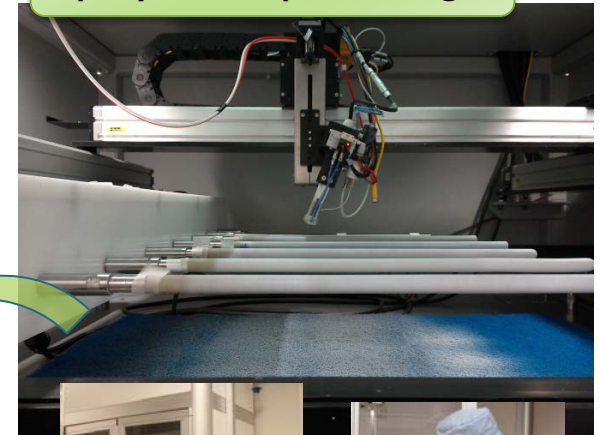
Dip-coating suspensions

NiO based paste

Extrusion of BZCY-NiO support

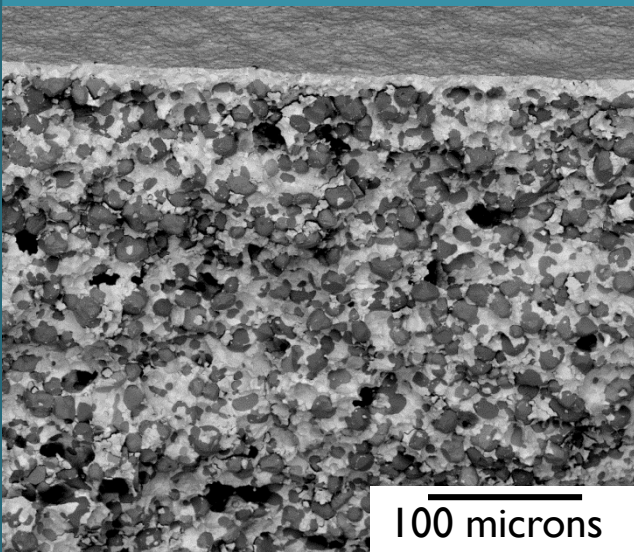


Spray- or dip-coating



Solid State Reactive Sintering

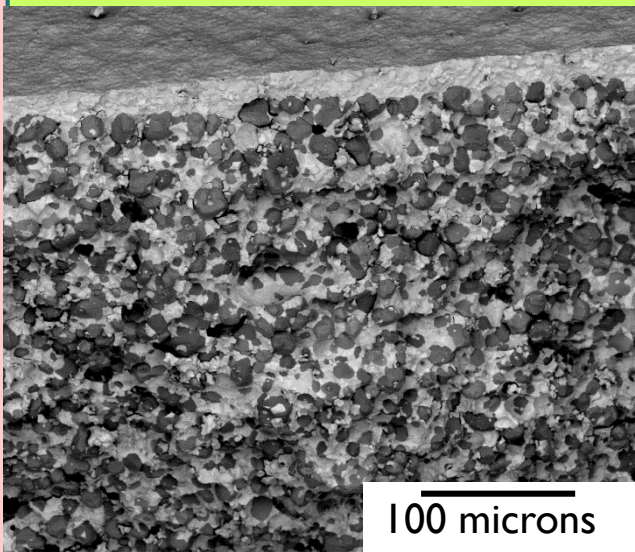




100 microns



100 microns

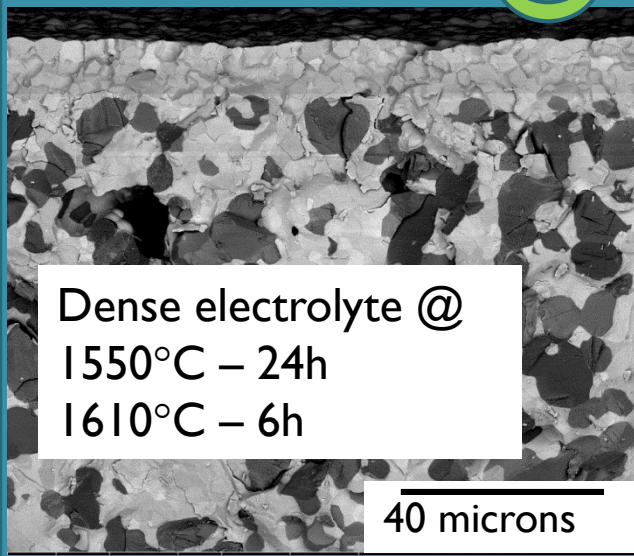


100 microns

BZCY72 // BZCY72-NiO 😊

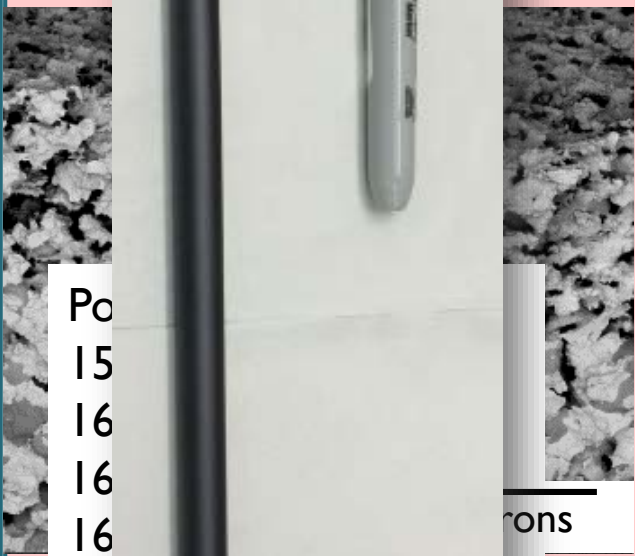
BZY

BZY10 // BZCY72-NiO 😊

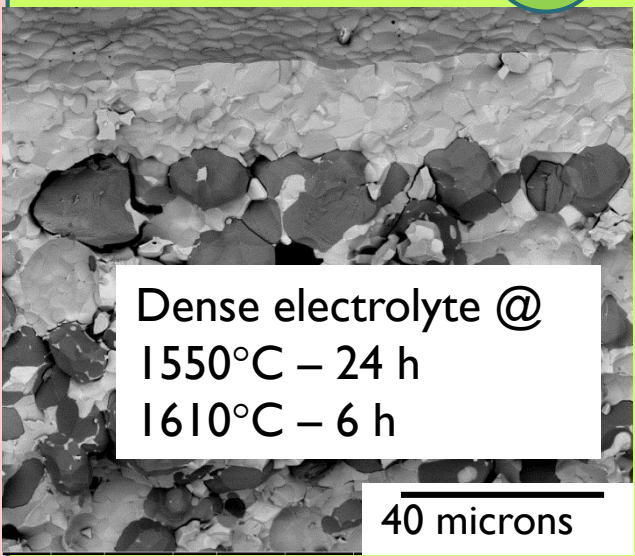


Dense electrolyte @
1550°C – 24h
1610°C – 6h

40 microns



40 microns



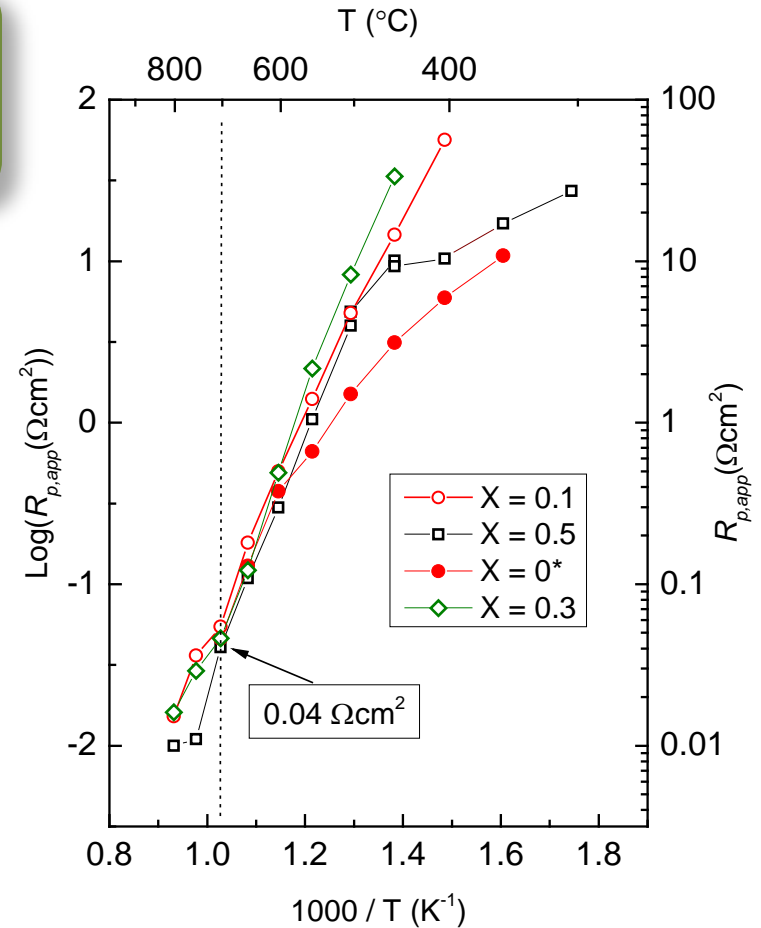
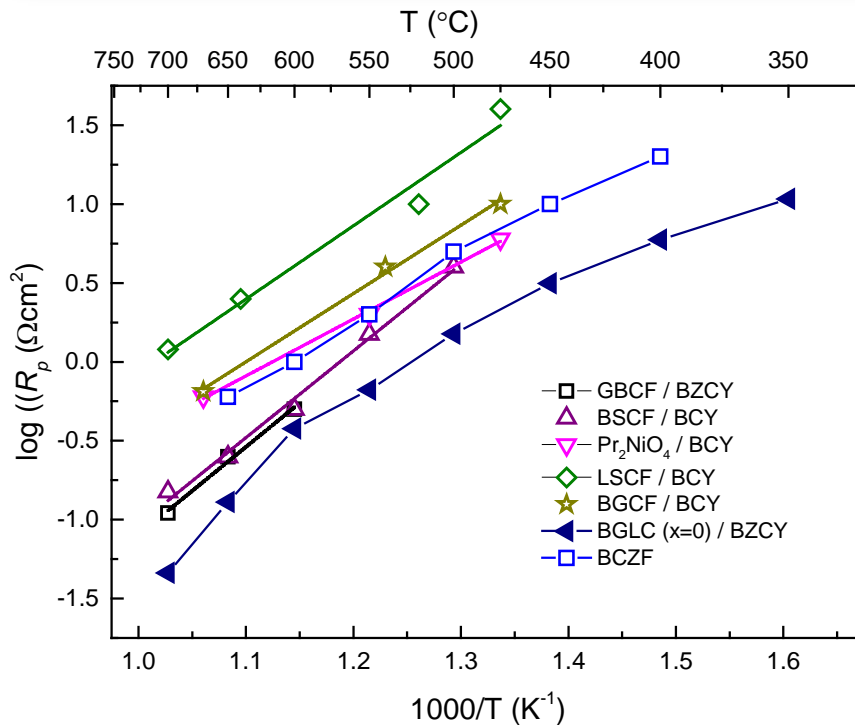
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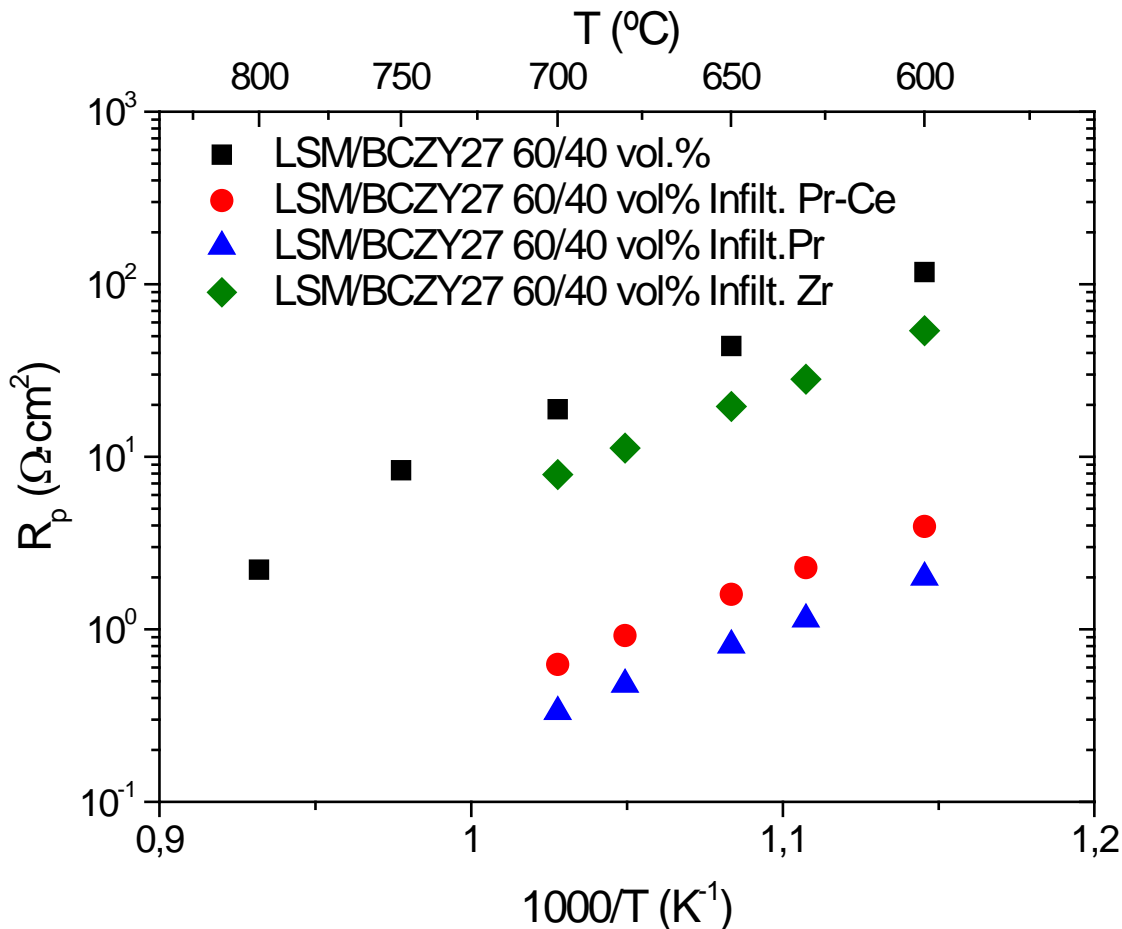
Development of new anode materials

$\text{Ba}_{1-x}\text{Gd}_{0.8}\text{La}_{0.2+x}\text{Co}_2\text{O}_{6-\delta}$ (BGLC) displays best PCE $\text{O}_2\text{-H}_2\text{O}$ -electrode performance (symmetrical disk samples)



LSM/BZCY composite electrodes

► Symmetrical cell LSM/BCZY 60/40 % vol.:



Conditions:

Total P= 3 bar

Steam 75%

T = 700 °C

Infiltration Pr-Ce

$R_p = 0.64 \Omega \cdot \text{cm}^2$ at 700 °C

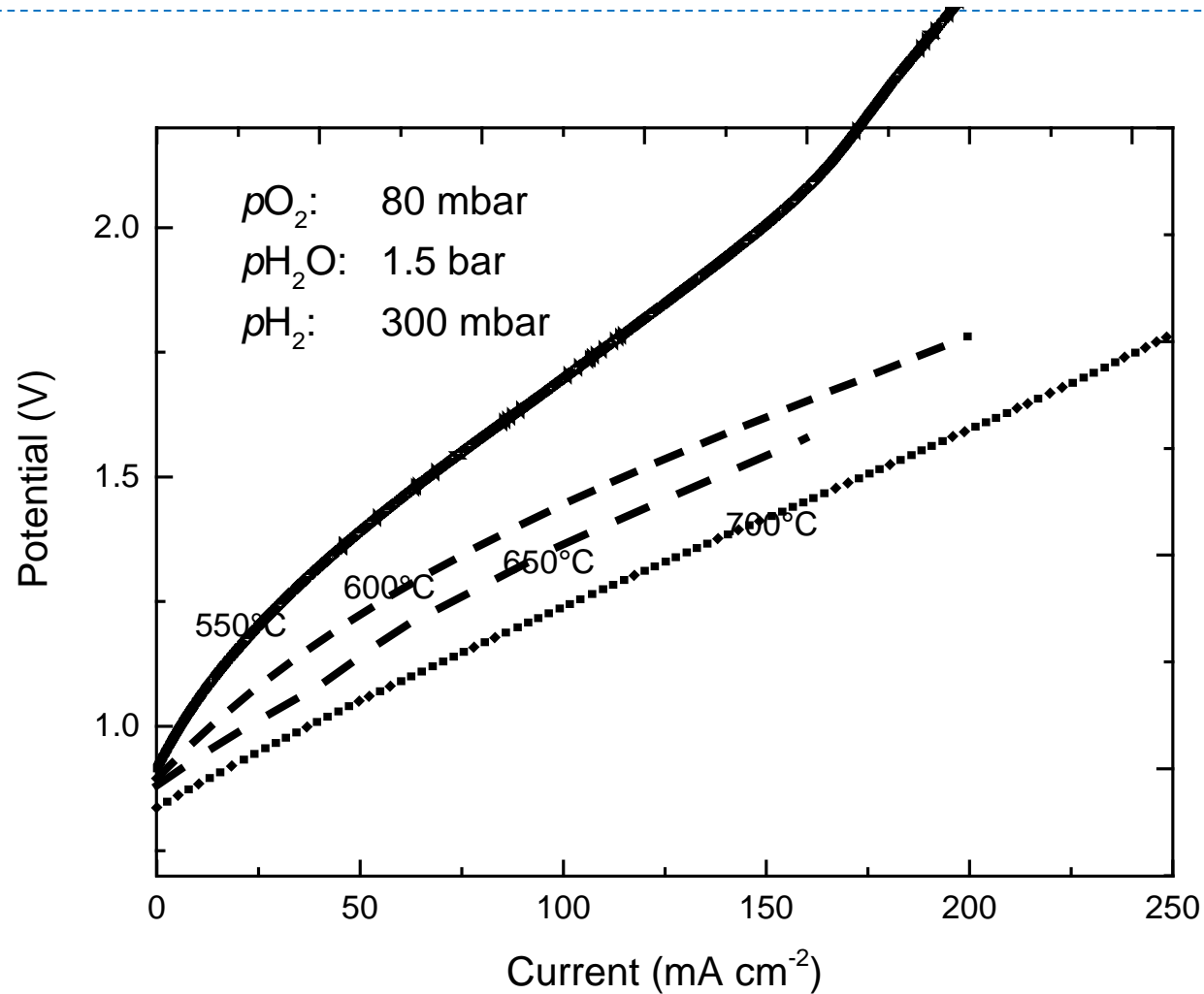
Infiltration Pr

$R_p = 0.33 \Omega \cdot \text{cm}^2$ at 700 °C

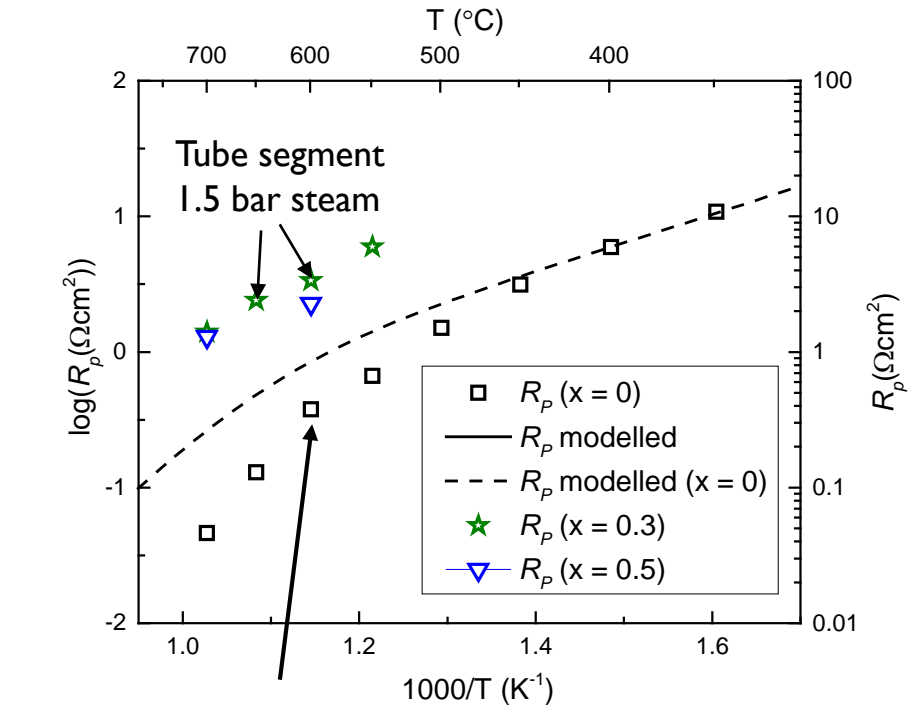
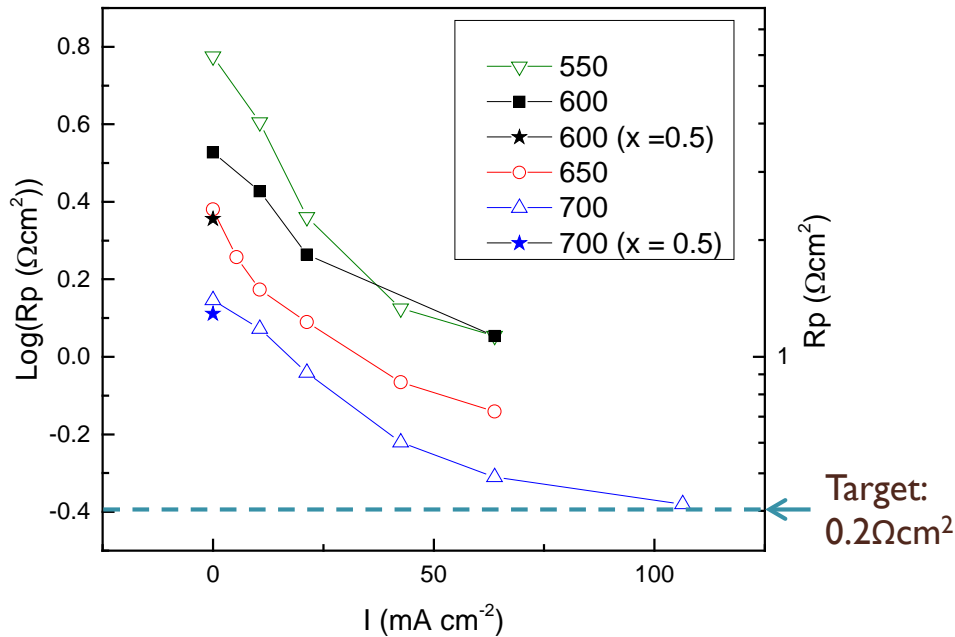
Infiltration Zr

$R_p = 7.88 \Omega \cdot \text{cm}^2$ at 700 °C

Electrolysis tests of single cell



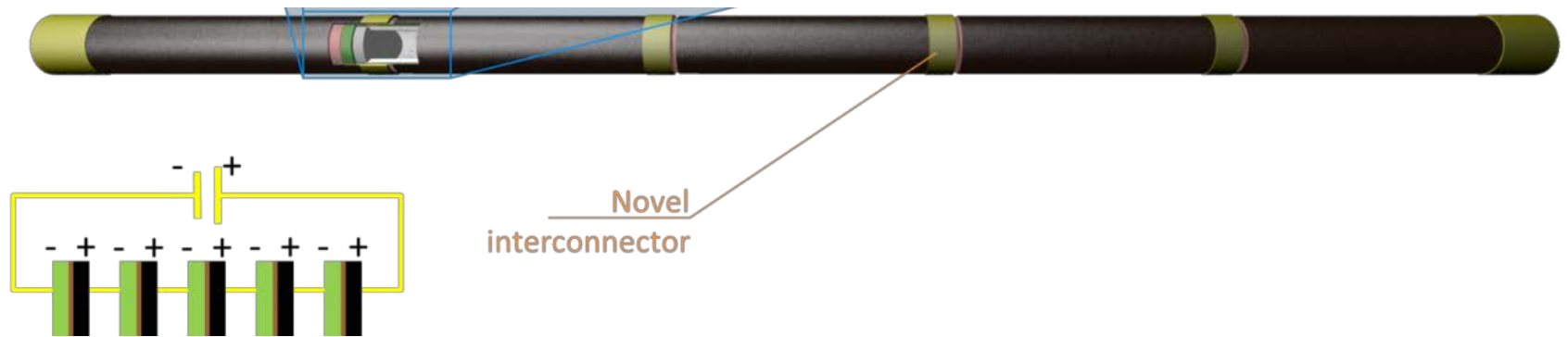
Electrode resistance an order of magnitude higher than expected values from button cell testing



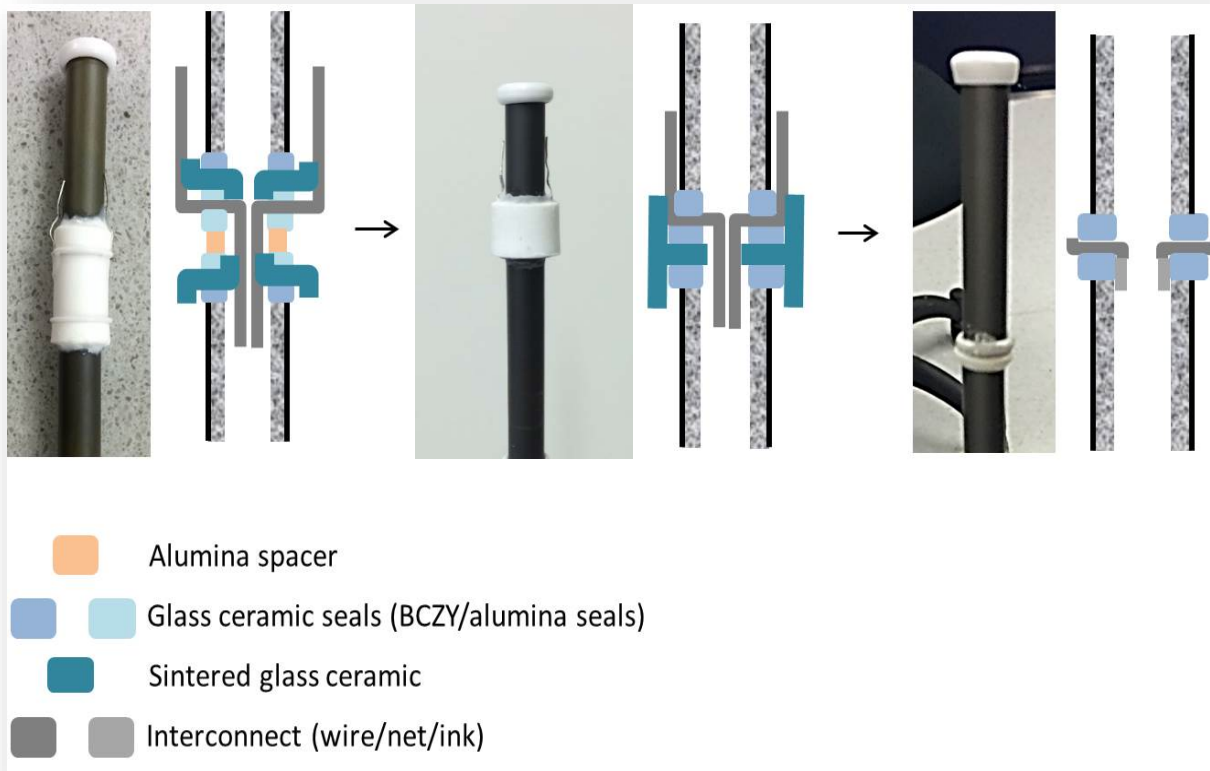
Button cell wet air

Scaling up – segmented-in-series tubes

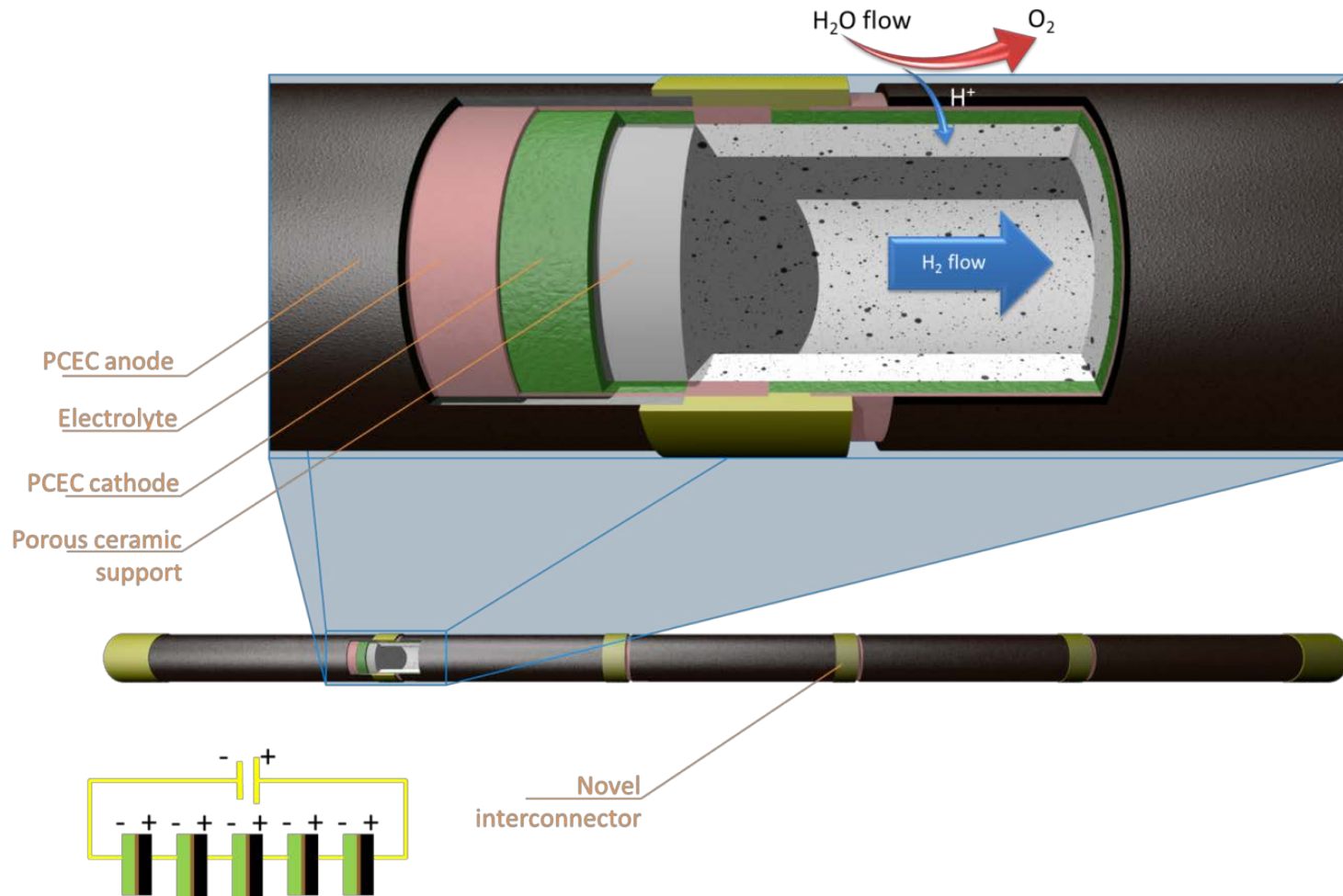
Higher tube voltage – lower tube current



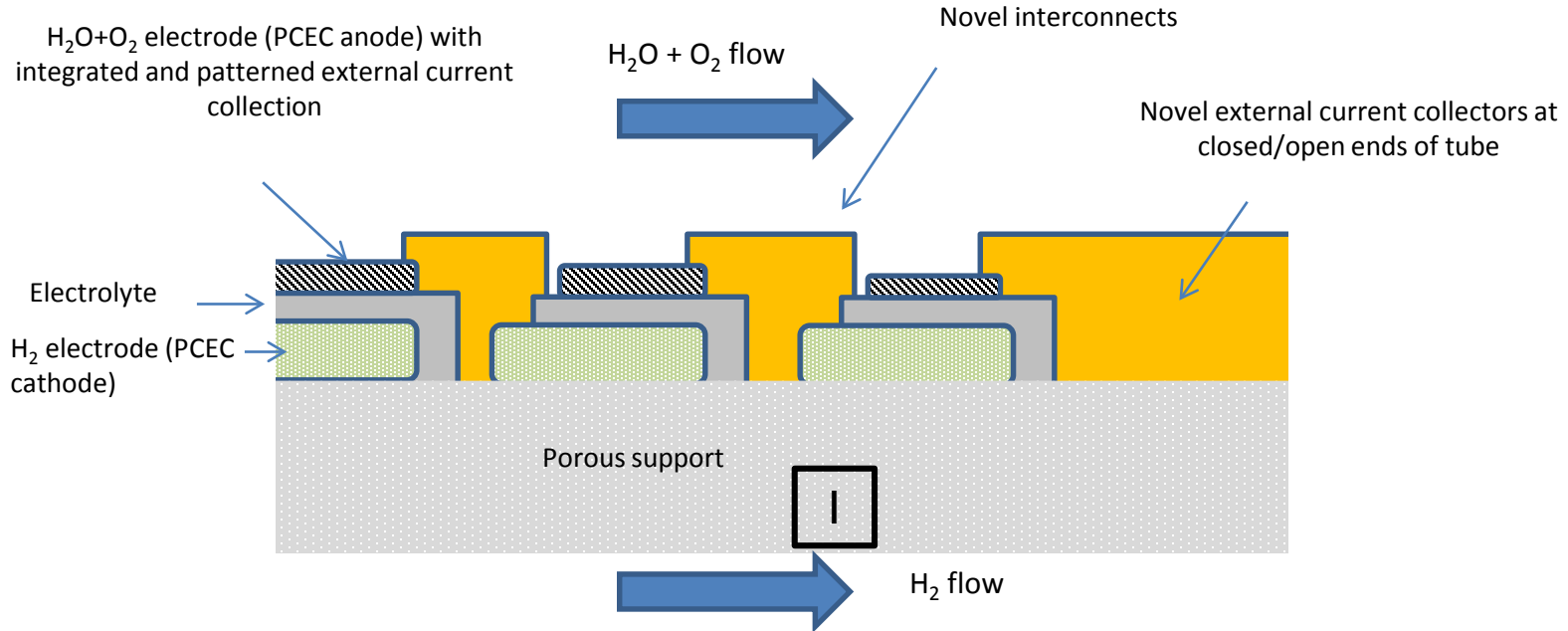
Scaling up – stacking individual segments



Scaling up – “Printing in series”



Segmented-in-series tubular cells

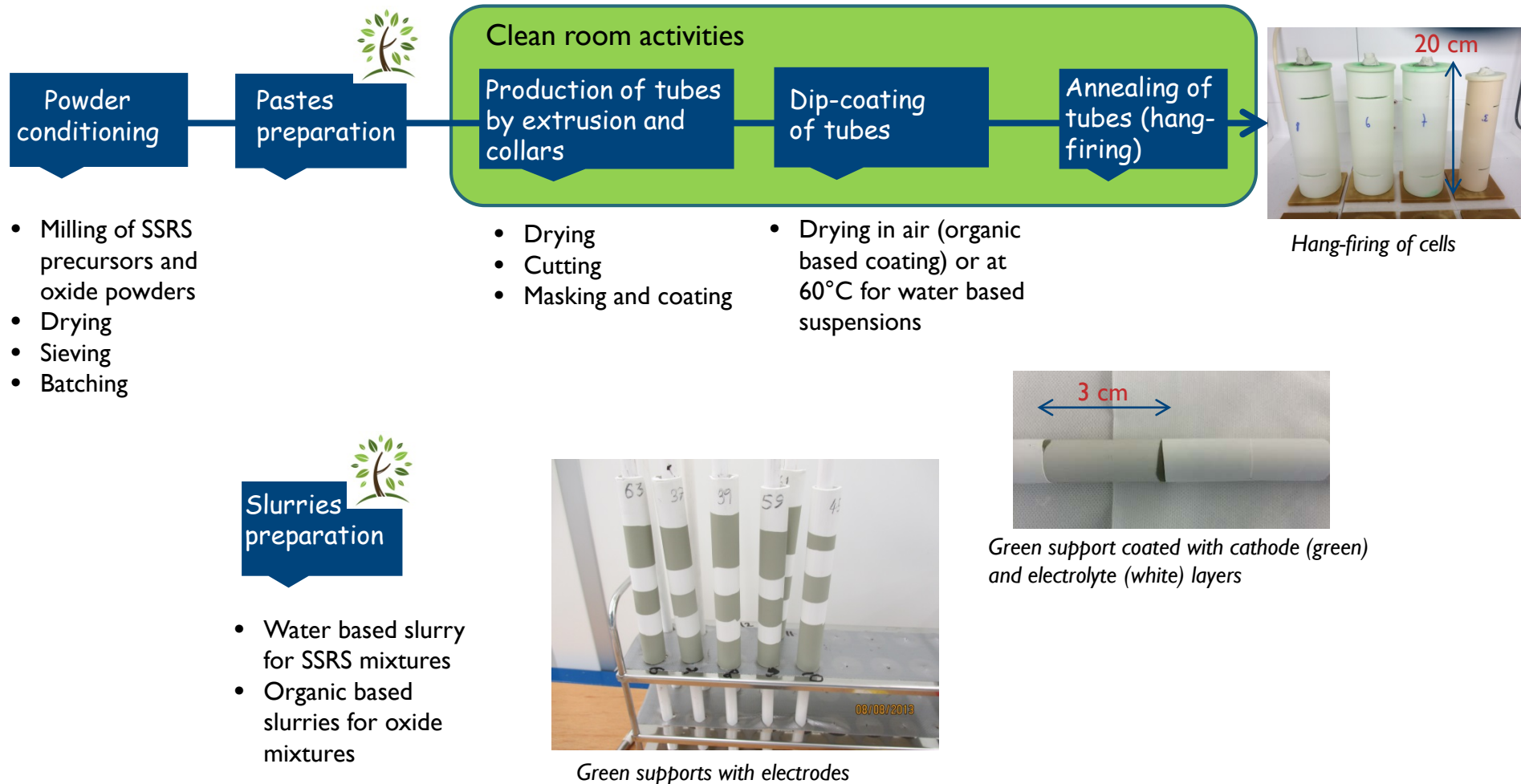


1 BZCY (SSRS) + sintering aid + pore formers

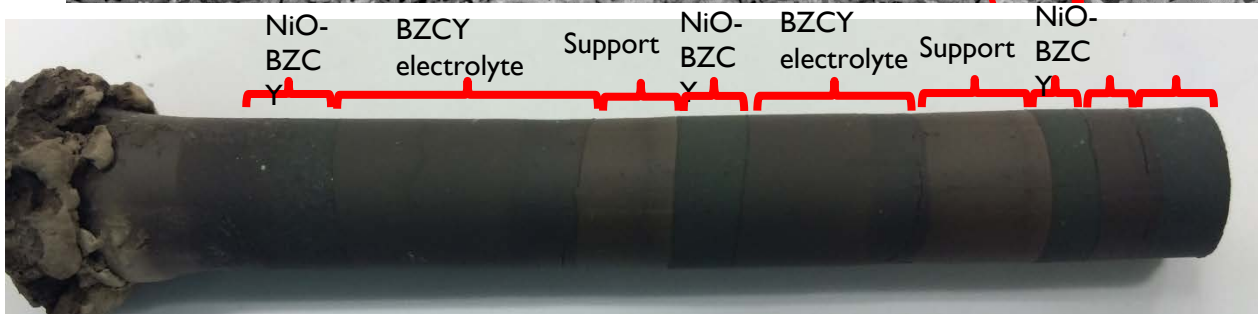
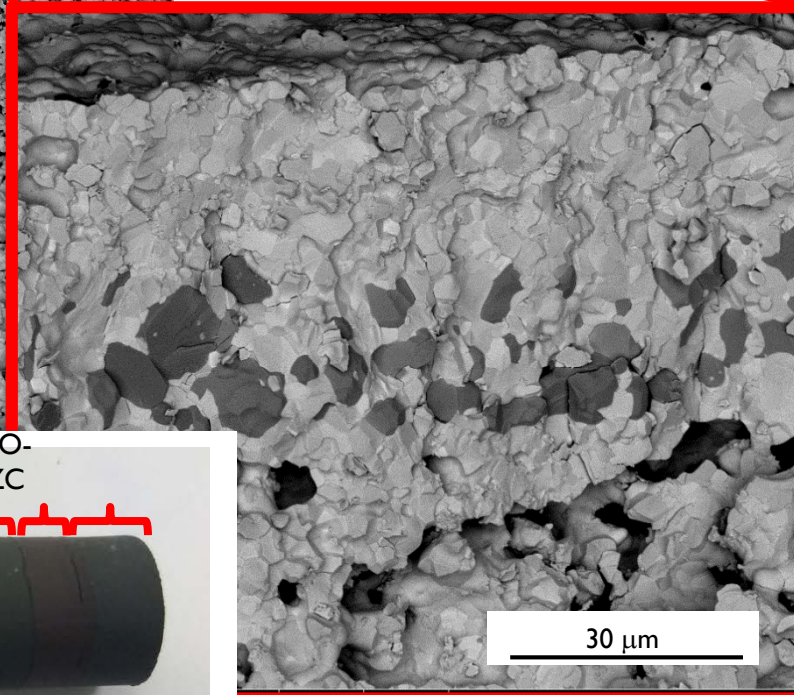
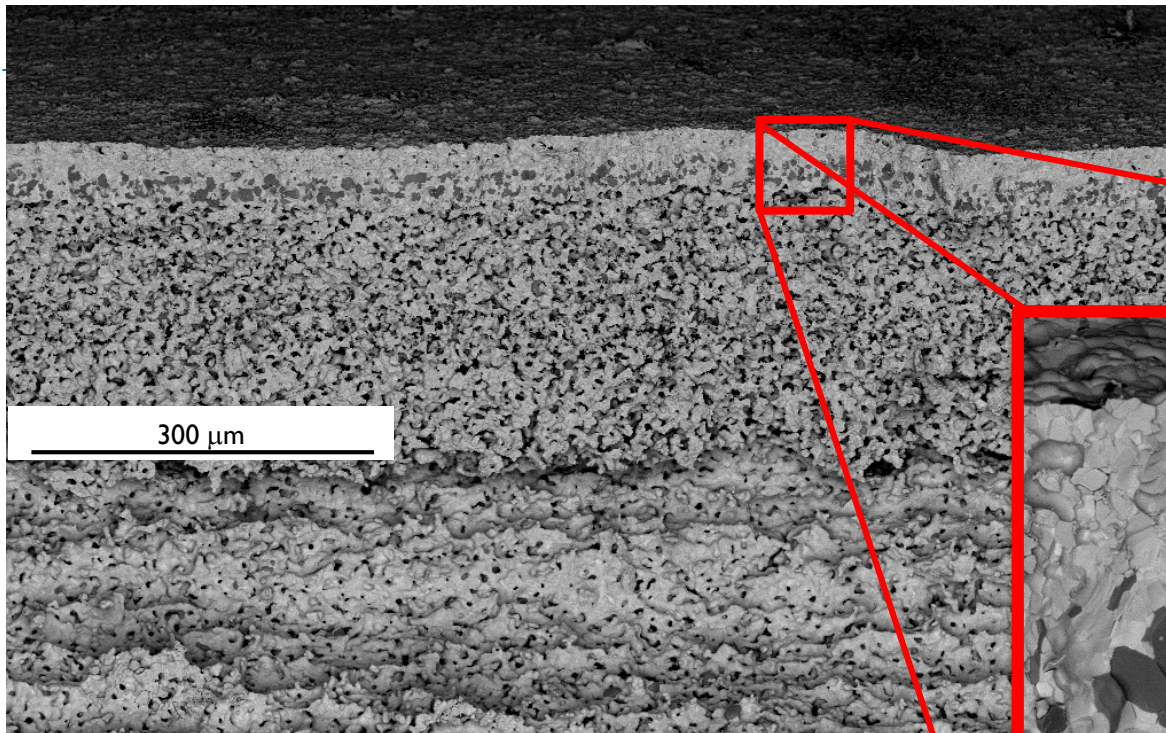
2 BZY10 (SSRS or oxide) or BZCY72 (SSRS or oxide) + NiO

3 BZCY72 or BZY10 (SSRS or oxide)

Manufacturing process



Optimized processing parameters for multi-layer sintering



Conclusions

- ▶ High temperature proton ceramic electrolyzers can produce dry, pressurized hydrogen
- ▶ Processing and manufacturing of tubular half cells is now well established
- ▶ State-of-the-art electrolyser anodes are developed on button cell scale
 - ▶ Deposition and firing protocols for tubular cells currently being developed
- ▶ Segmented-in-series tubular cells are needed to reduce total current of tubes in real operational conditions



Acknowledgements



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