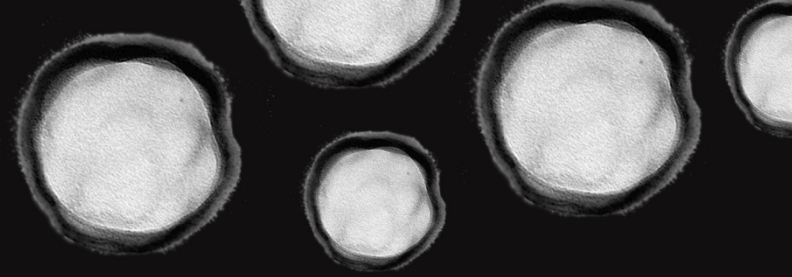




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Anode performance based on high temperature proton conducting electrolyzers and a multitube module construction



idhea

N. Bausá, M. Tarach and J.M. Serra

International discussion on hydrogen energy and applications
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Outline

- ✓ Introduction
- ✓ Installation of the high pressure set-up
- ✓ Compatibility and stability tests of the selected anode material
 - Under 3 bars air + H₂O (75% steam) at 700 °C for 72 h
- ✓ Symmetrical cells EIS:
 - LSM/BCZY27 (50/50 and 60/40 vol.%)
 - Study by changing p_{H_2O} , p_{O_2} and p_T
 - Infiltrations (Pr-Ce, Pr, Ce, Zr)
- ✓ Multitube module design
- ✓ Conclusions



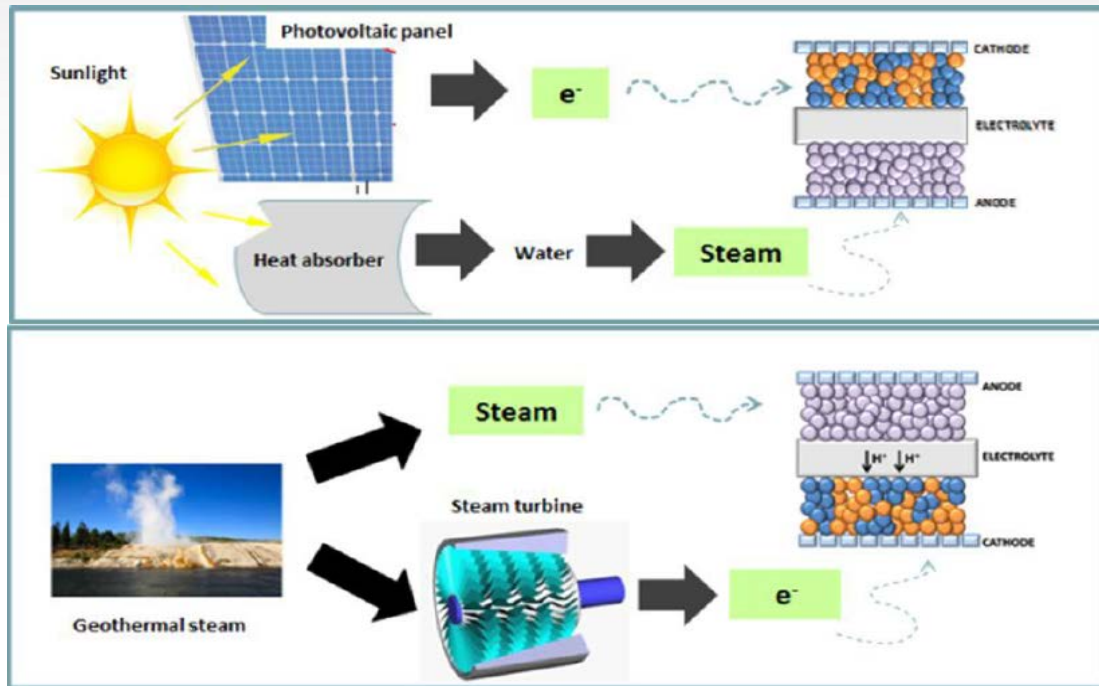
Introduction



Introduction

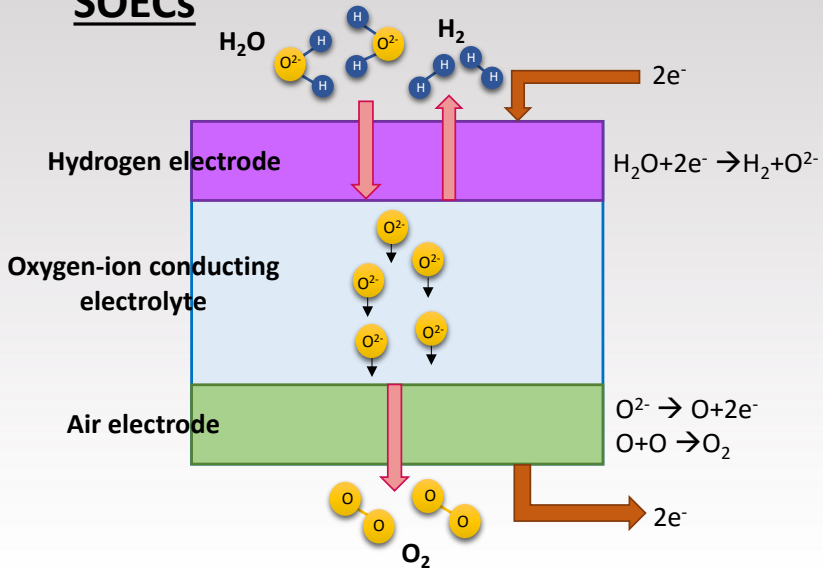
➤ The ELECTRA project:

- Scalable fabrication of tubular HTE cells with proton conducting electrolytes for production of H_2 from steam and renewable sources (solar, wind, geothermal, etc.)



Introduction

SOECs

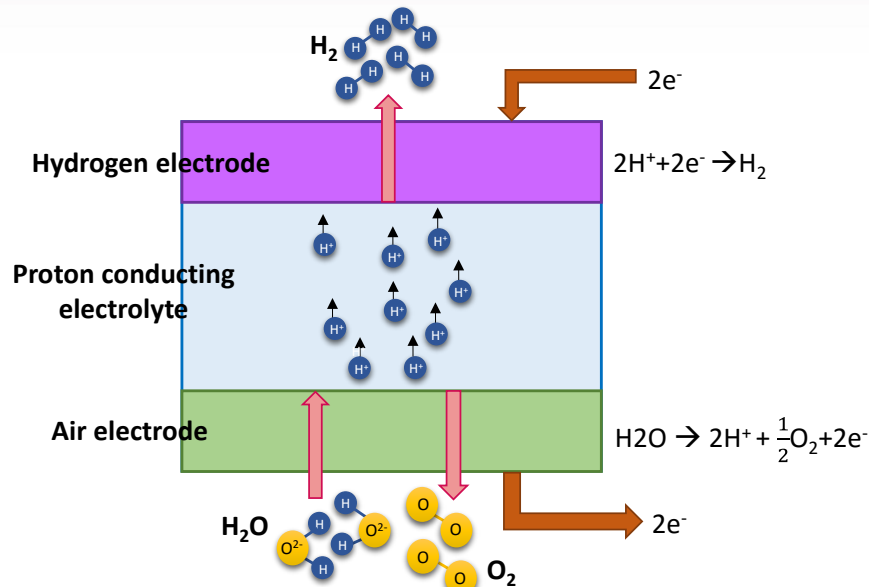


- Utilise steam and heat procedures
- Produce wet H₂
- Delamination of anode
- High operation temperatures (>800 °C)
- Technology more investigated



PCECs

- Utilise steam and heat procedures
- Produce dry H₂ directly
- No anode delamination
- Low operation temperatures (<700 °C)
- Technology less investigated
- Materials still in development



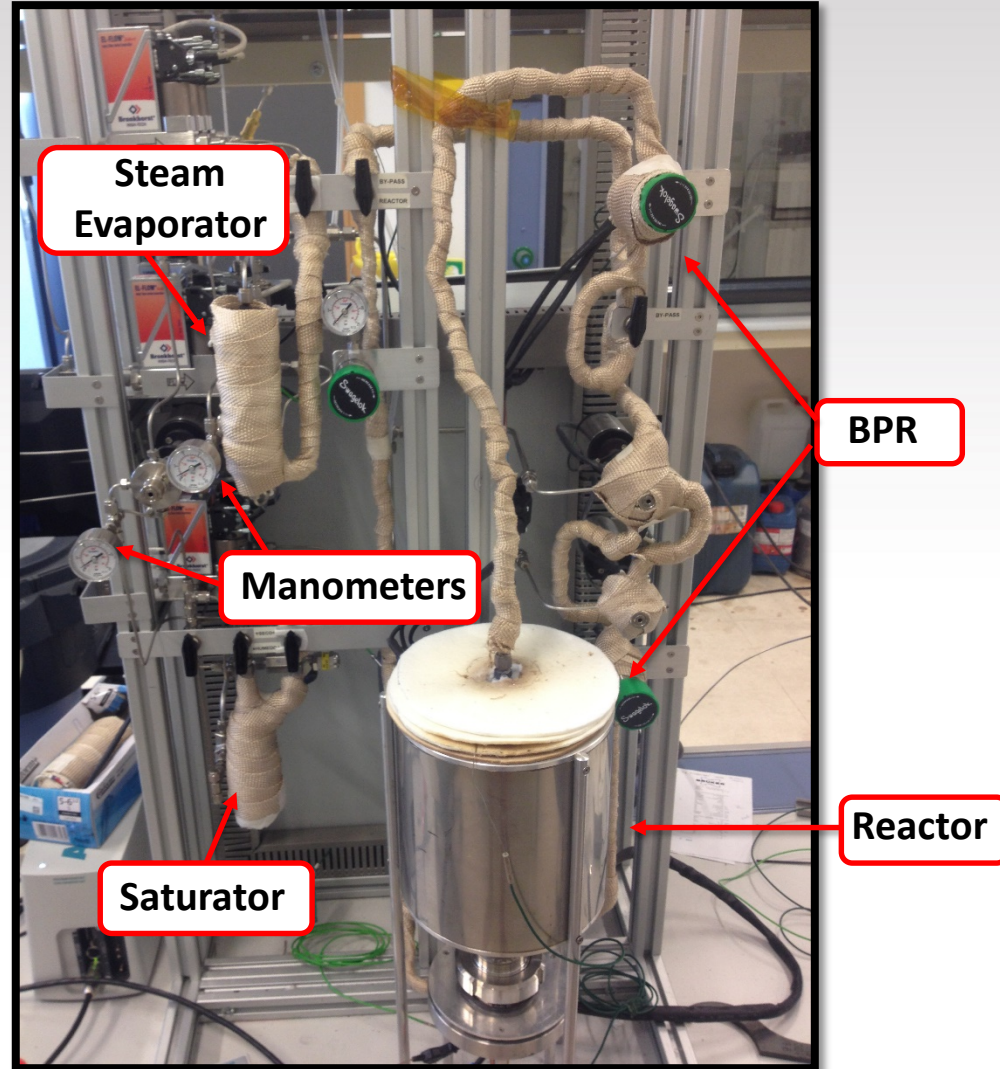
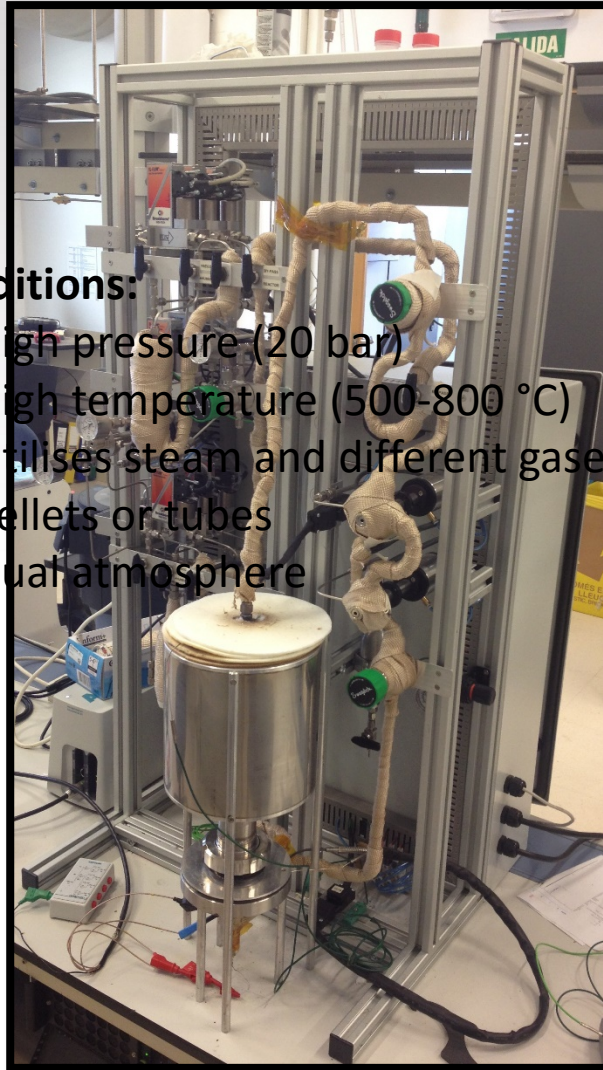
Installation of the high pressure set up



Installation of the high pressure set up

Conditions:

- High pressure (20 bar)
- High temperature (500-800 °C)
- Utilises steam and different gases
- Pellets or tubes
- Dual atmosphere



Compatibility and stability tests of the selected anode material



Compatibility tests with BCZY27

Electrolyte material

BCZY27: $\text{BaCe}_{0.2}\text{Zr}_{0.7}\text{Y}_{0.1}\text{O}_3$

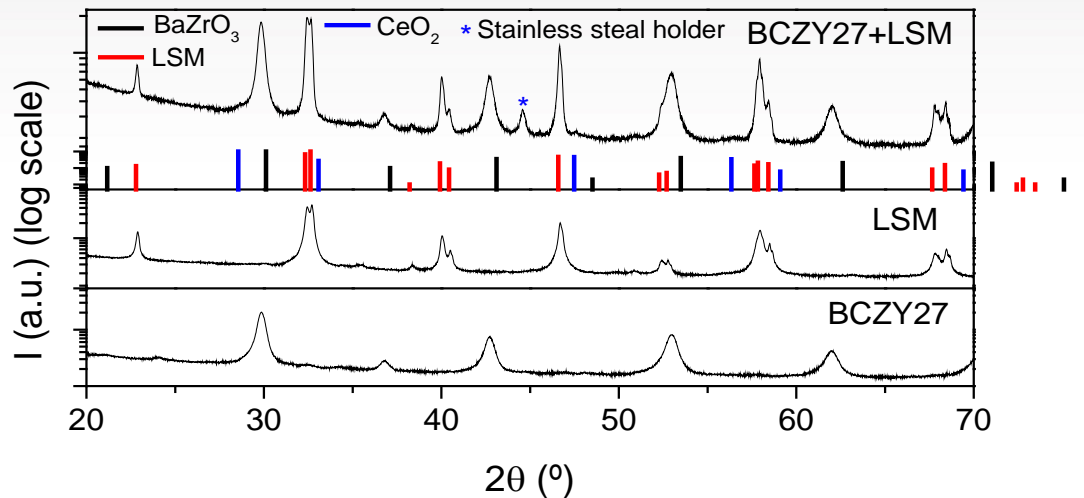
Possible Steam
Electrode material

LSM: $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$

Testing T, t (dry)

1100 °C/5 h

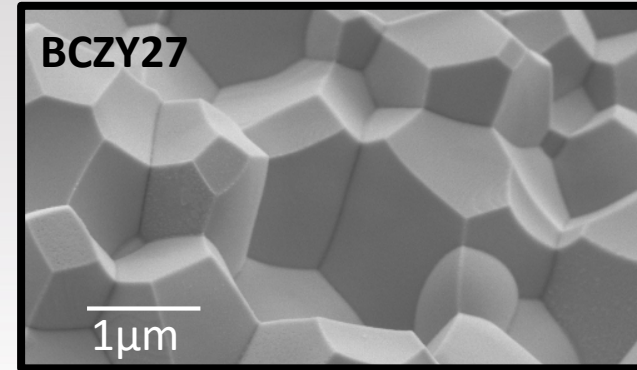
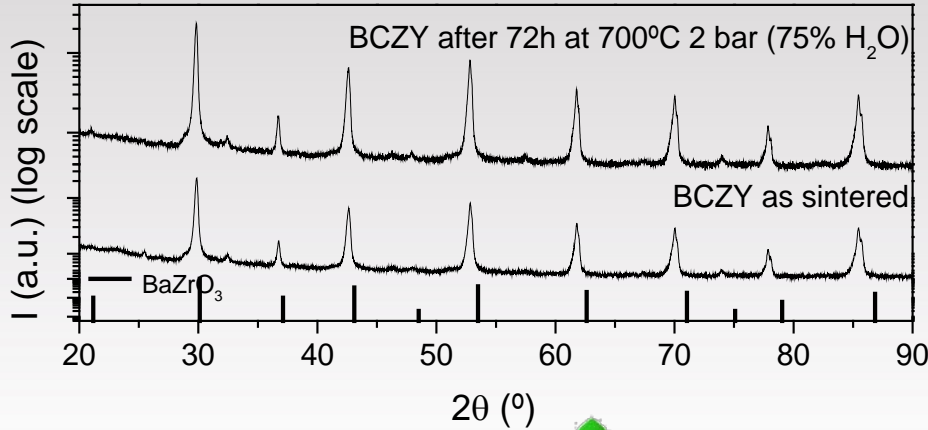
LSM: $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$



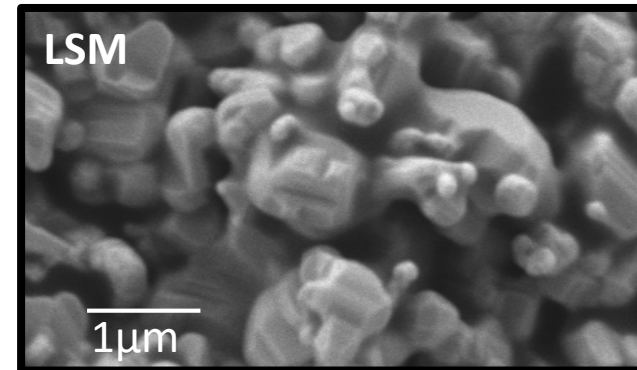
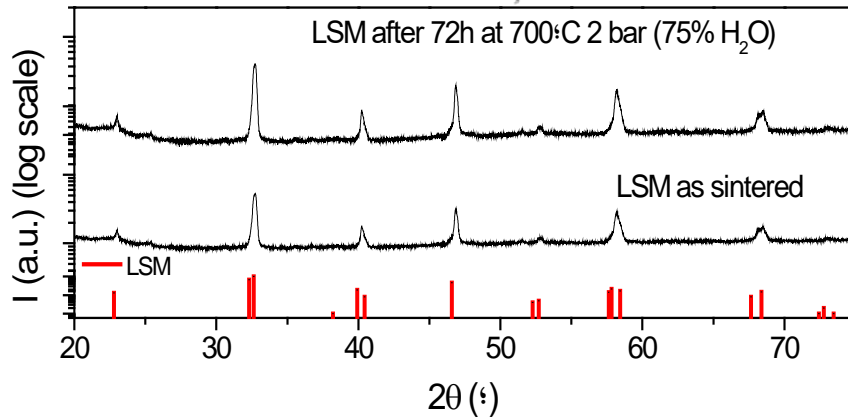
CeO₂ segregation also observed in BCZY27 after long times or higher sintering T

Stability tests under operating conditions

BCZY: $\text{BaCe}_{0.2}\text{Zr}_{0.7}\text{Y}_{0.1}\text{O}_3$



LSM: $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$



3 bar air + H₂O (75% steam) at 700 °C for 72 h

Symmetrical cells EIS



Symmetrical cells EIS

➤ LSM/BCZY27

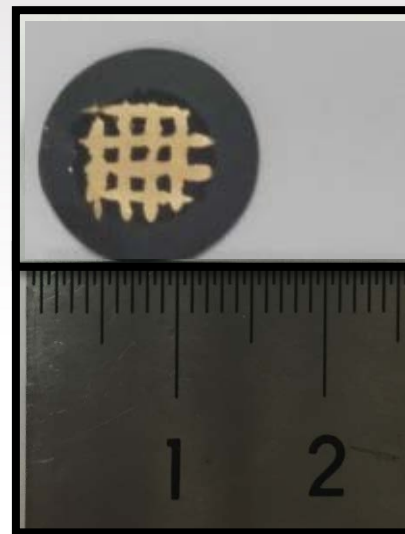
✓ Infiltrations:

1. Pr – Ce (50 % vol.) [2M] 850 °C/2h
2. Pr [2M] 850 °C/2h
3. Ce[2M] 850 °C/2h
4. Zr [2M] 850 °C/2h

Electrolyte: BCZY27

Electrode: LSM/BCZY27 50 vol. %

Current collector: Au



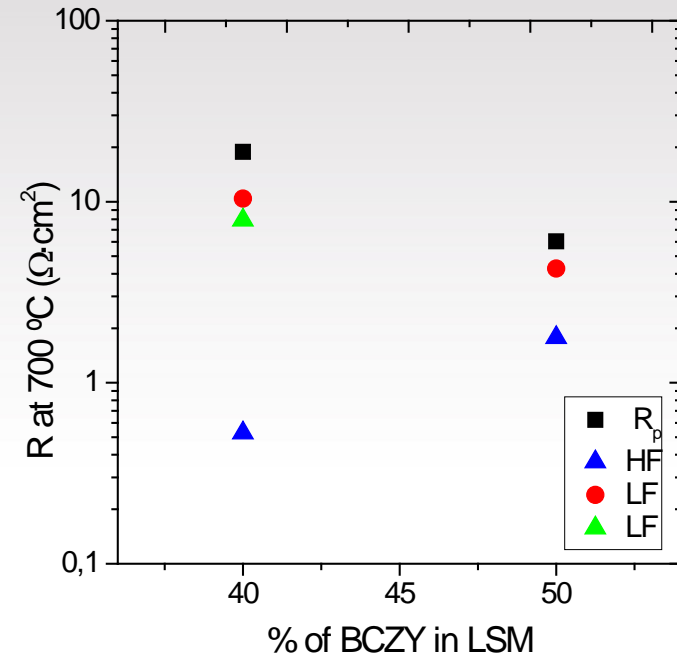
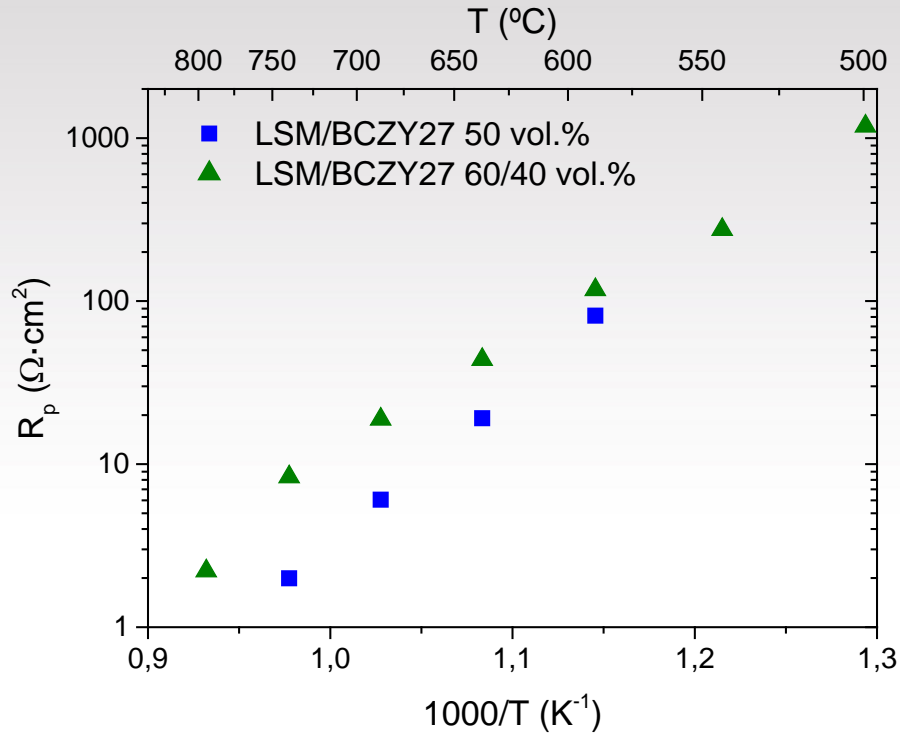
$\varnothing_{\text{electrolyte}} = 14 \text{ mm}$

$\varnothing_{\text{electrode}} = 9 \text{ mm}$

Thickness = 1.6 mm

Symmetrical cells EIS

LSM/BCZY composite



Conditions:

Total P= 3 bar

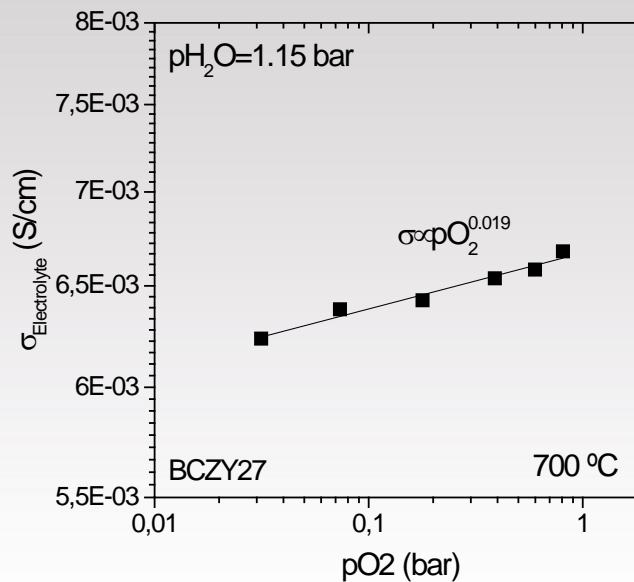
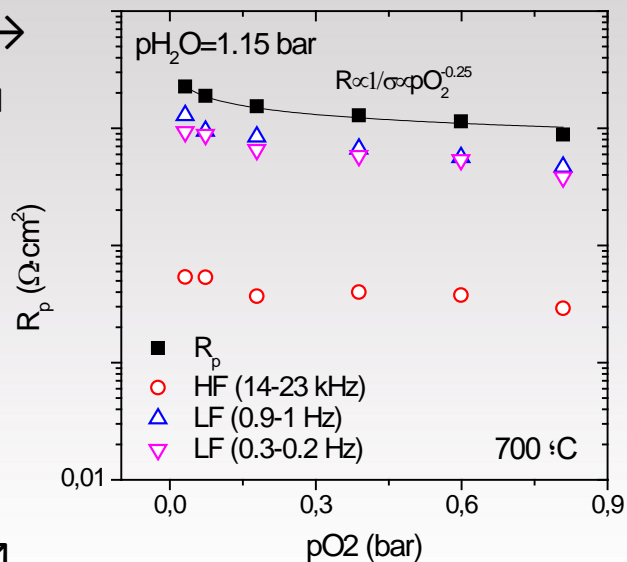
Steam 75%

3 days

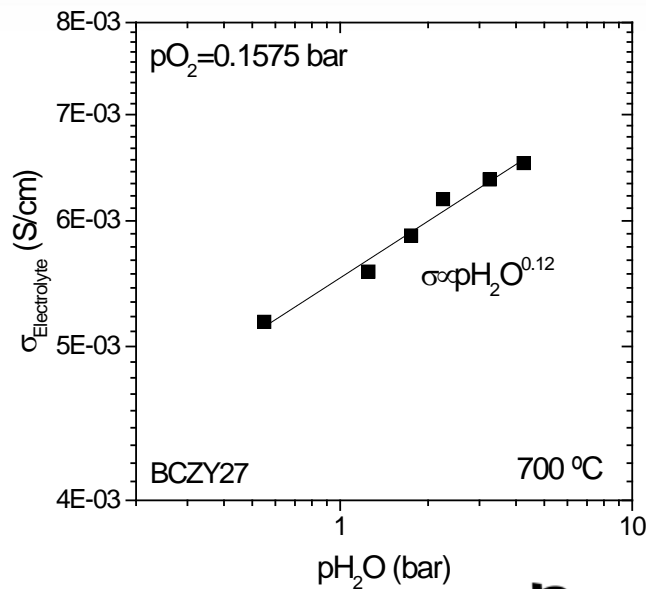
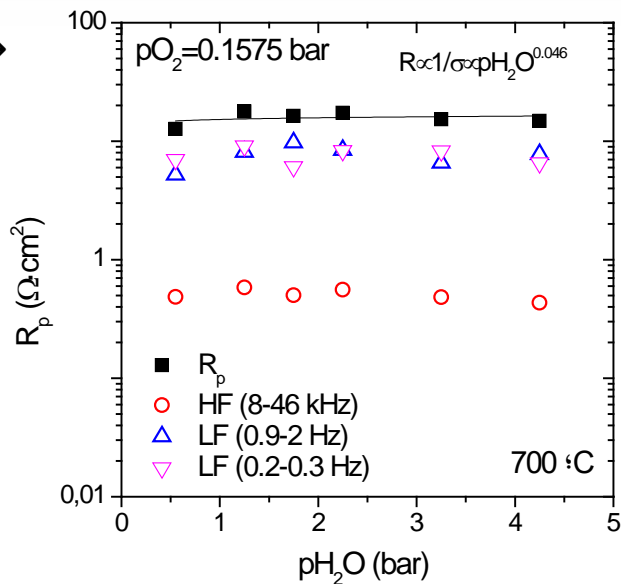


LSM/BCZY study by changing steam pressure, pO_2 and p_T

a) $p_{H_2O} \rightarrow$
 $p_{O_2} \nearrow$
 $p_T \nearrow$



b) $p_{H_2O} \nearrow$
 $p_{O_2} \rightarrow$
 $p_T \nearrow$

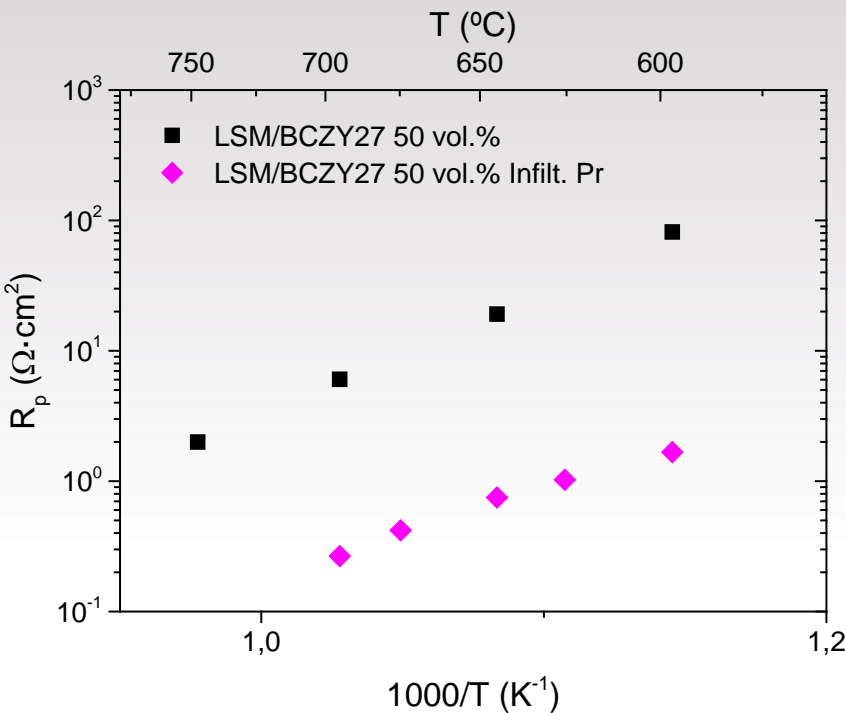


Infiltrations in LSM/BCZY



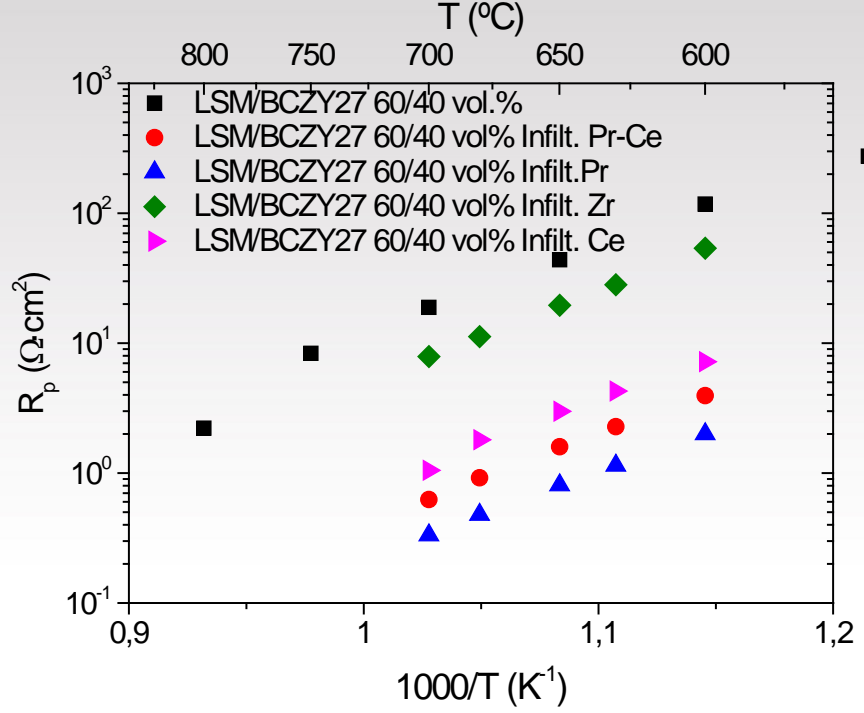
Symmetrical cells LSM/BCZY - Infiltrations

LSM/BCZY 50 vol. %



Infiltration Pr
 $R_p = 0.27 \Omega \cdot \text{cm}^2$ at 700 °C

LSM/BCZY 60/40 vol. %



Infiltration Pr-Ce
 $R_p = 0.64 \Omega \cdot \text{cm}^2$ at 700 °C

Infiltration Pr
 $R_p = 0.33 \Omega \cdot \text{cm}^2$ at 700 °C

Infiltration Ce
 $R_p = 1.04 \Omega \cdot \text{cm}^2$ at 700 °C

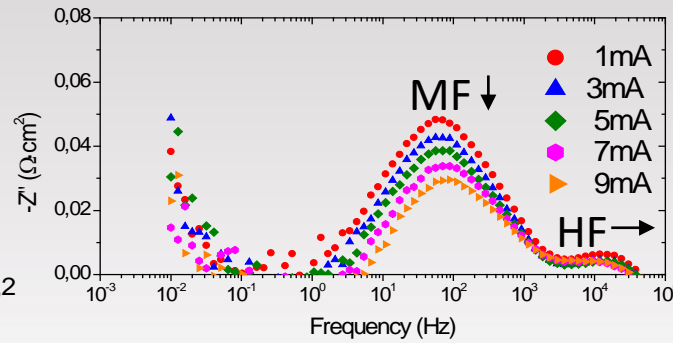
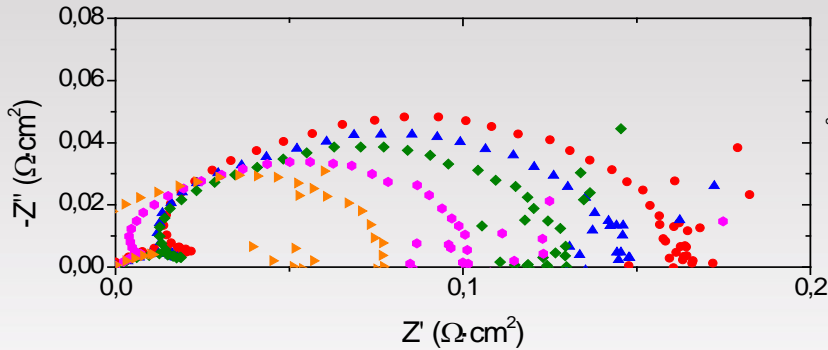
Infiltration Zr
 $R_p = 7.88 \Omega \cdot \text{cm}^2$ at 700 °C

Conditions:
 Total P= 3 bar
 Steam 75%
 T = 700 °C



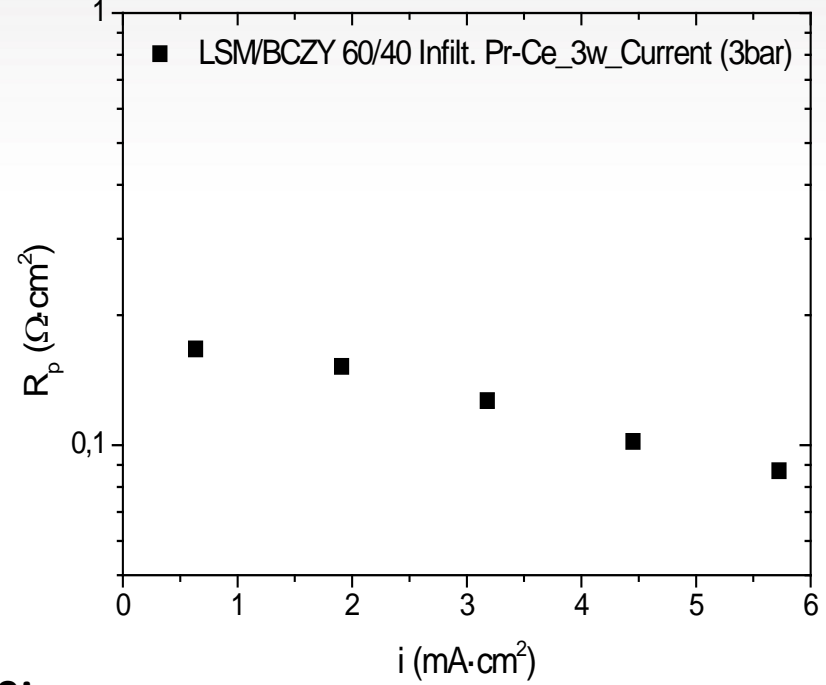
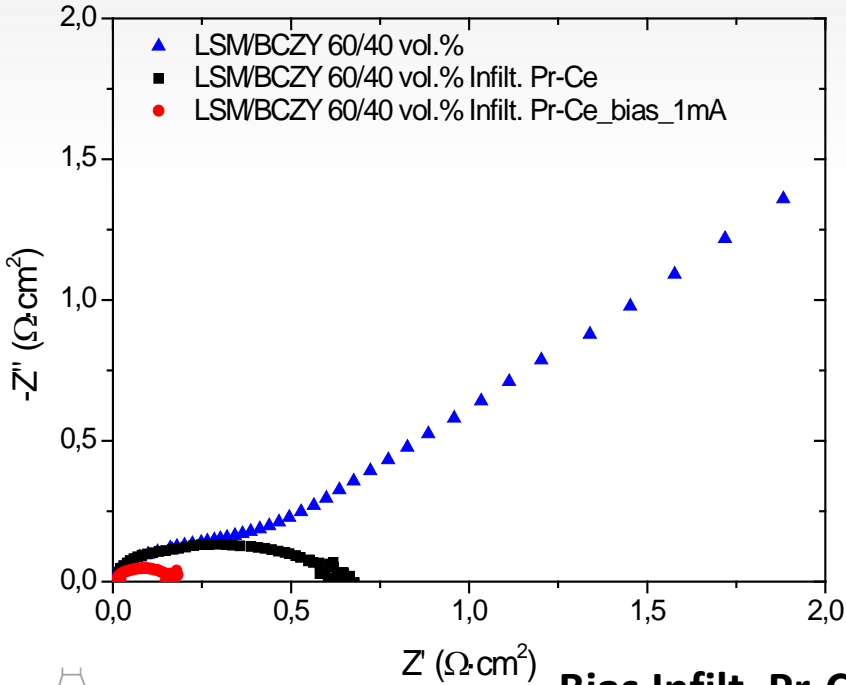
Bias – Infiltrations in LSM/BCZY 60/40 vol. %

Infiltration Pr-Ce 850 °C in LSM/BCZY 60/40 vol. %



Conditions:
 Total P = 3 bar
 Steam 75%
 T = 700 °C

- 1mA
- ▲ 3mA
- ◆ 5mA
- 7mA
- ▲ 9mA



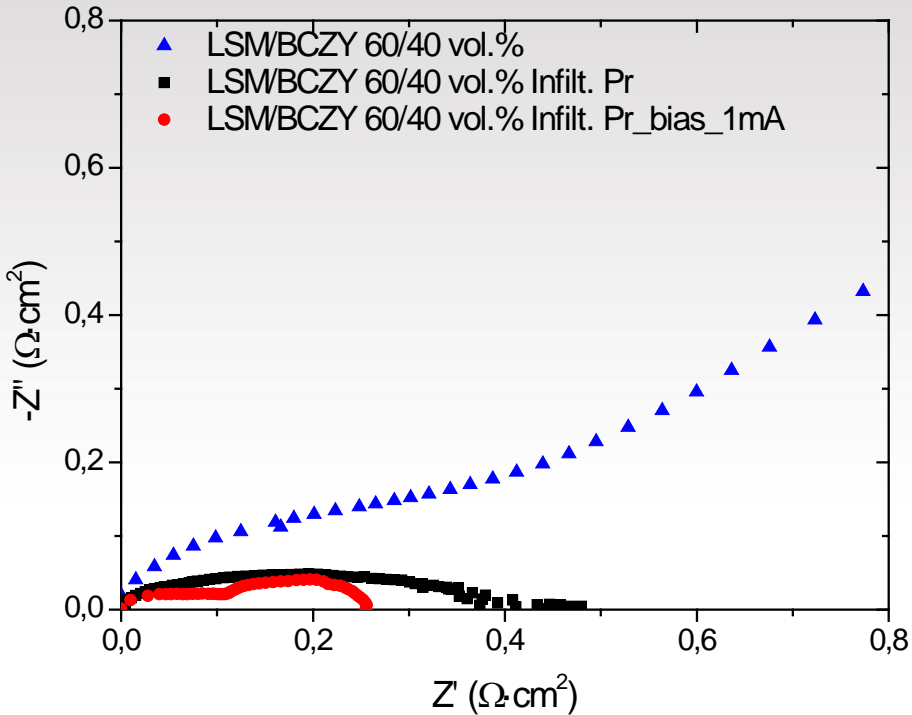
Bias Infiltr. Pr-Ce:

$i = 0.63 \text{ mA/cm}^2 \rightarrow R_p = 0.17 \text{ } \Omega \cdot \text{cm}^2$
 $i = 5.7 \text{ mA/cm}^2 \rightarrow R_p = 0.087 \text{ } \Omega \cdot \text{cm}^2$

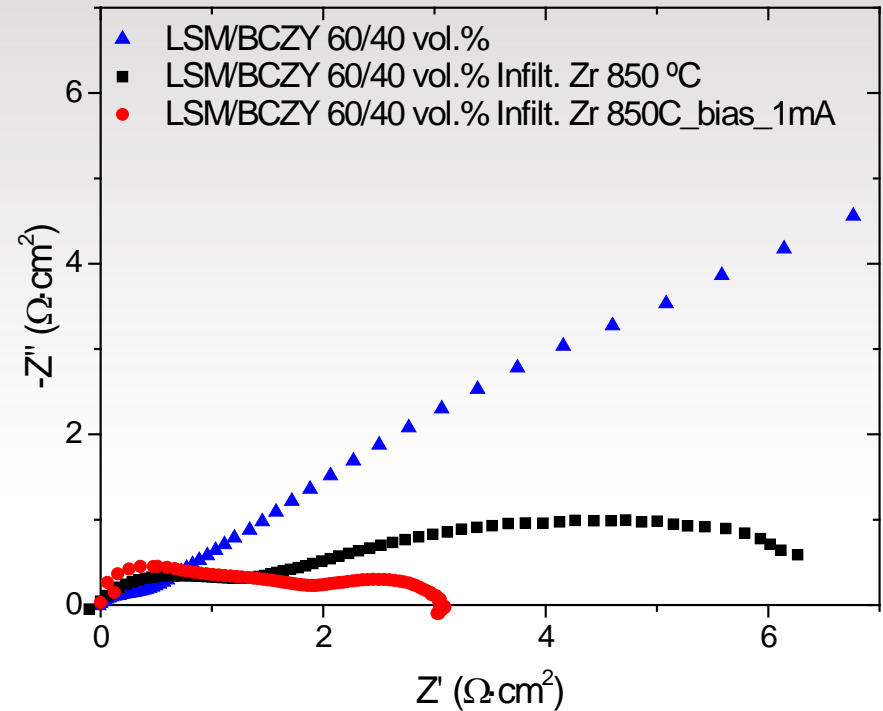


Bias – Infiltrations in LSM/BCZY 60/40 vol. %

Infiltration Pr 850 °C in LSM/BCZY



Infiltration Zr 850 °C in LSM/BCZY



Bias Infiltr. Pr:

$$i = 0.63 \text{ mA/cm}^2 \rightarrow R_p = 0.27 \text{ } \Omega \cdot \text{cm}^2$$

$$i = 3.2 \text{ mA/cm}^2 \rightarrow R_p = 0.18 \text{ } \Omega \cdot \text{cm}^2$$

Bias Infiltr. Zr:

$$i = 0.63 \text{ mA/cm}^2 \rightarrow R_p = 2.53 \text{ } \Omega \cdot \text{cm}^2$$

$$i = 6.99 \text{ mA/cm}^2 \rightarrow R_p = 1.01 \text{ } \Omega \cdot \text{cm}^2$$

Conditions:

Total P= 3 bar

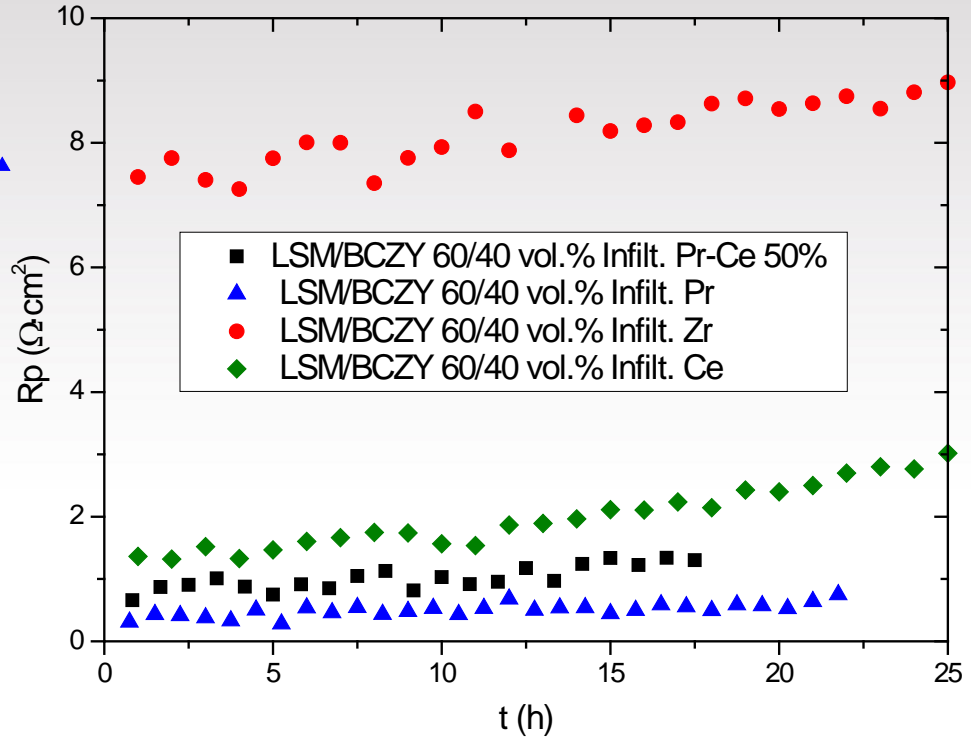
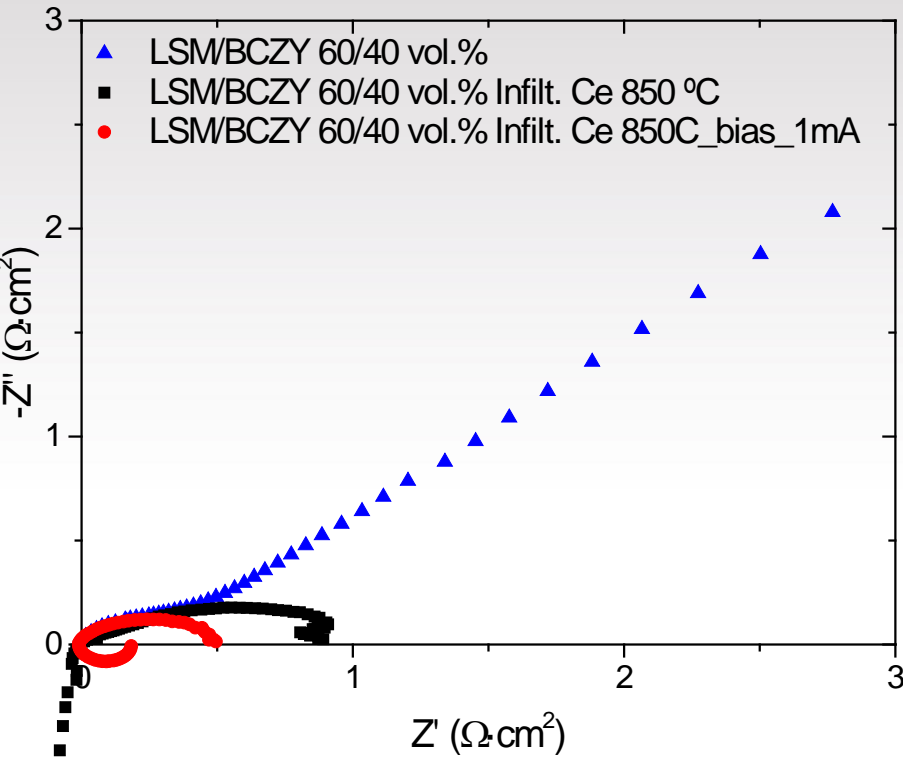
Steam 75%

T = 700 °C



Bias – Infiltrations in LSM/BCZY 60/40 vol. %

Infiltration Ce 850 °C in LSM/BCZY



Bias Infiltr. Ce:

$$i = 0.63 \text{ mA/cm}^2 \rightarrow R_p = 0.54 \text{ } \Omega \cdot \text{cm}^2$$

$$i = 5.72 \text{ mA/cm}^2 \rightarrow R_p = 0.05 \text{ } \Omega \cdot \text{cm}^2$$

Conditions:

Total P= 3 bar

Steam 75%

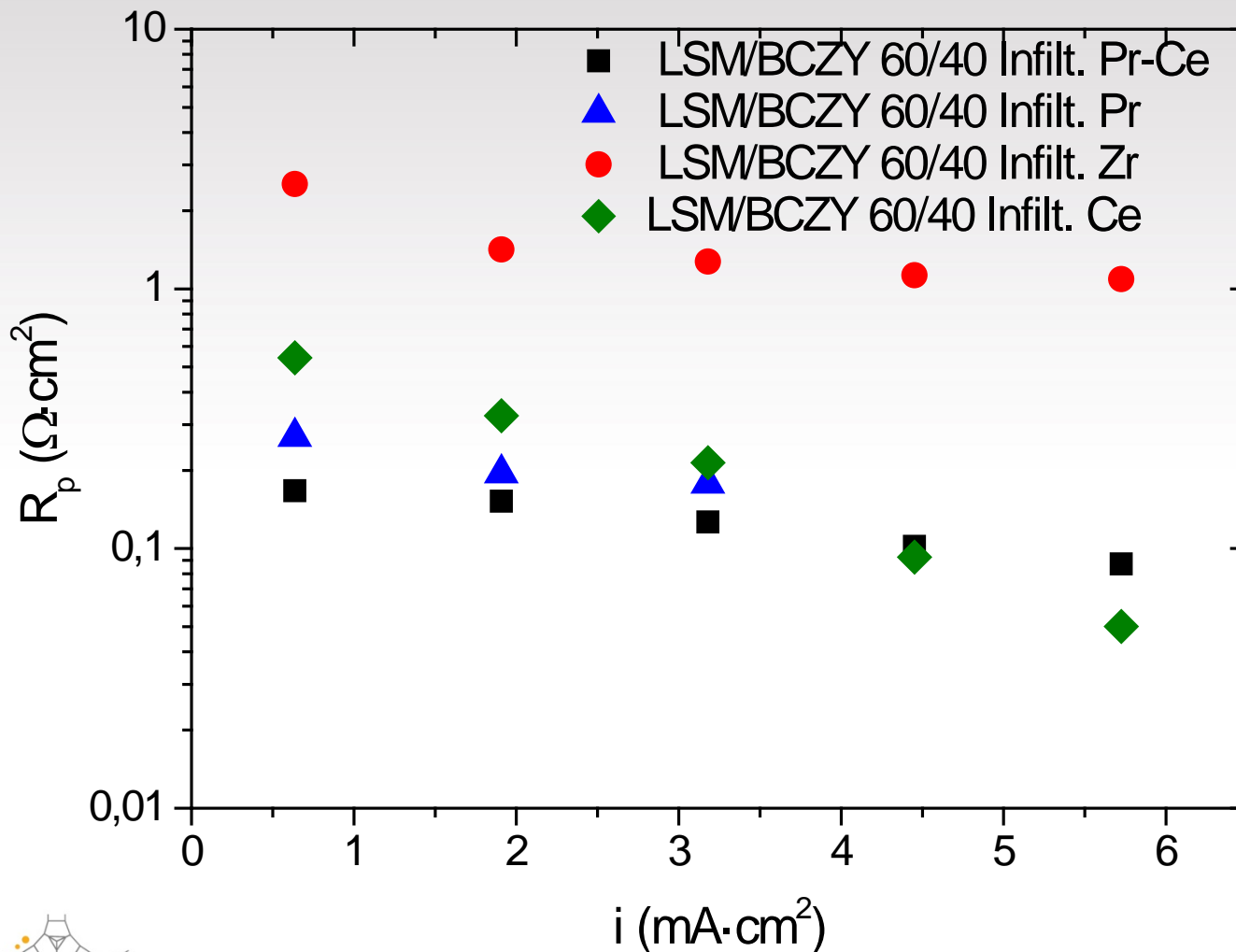
T = 700 °C

Good stability!



Comparative infiltrations

Infiltrations in LSM/BCZY 60/40 vol. %



Conditions:

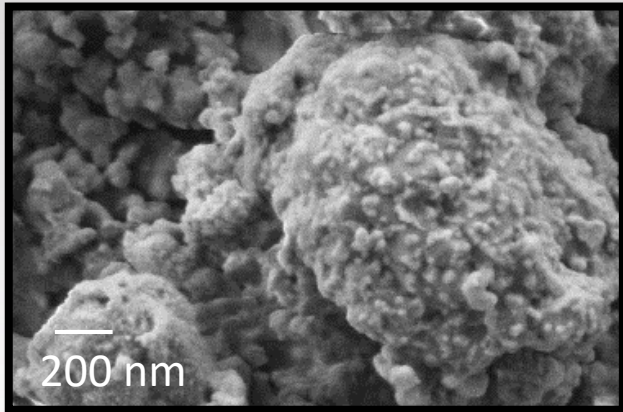
Total P= 3 bar

Steam 75%

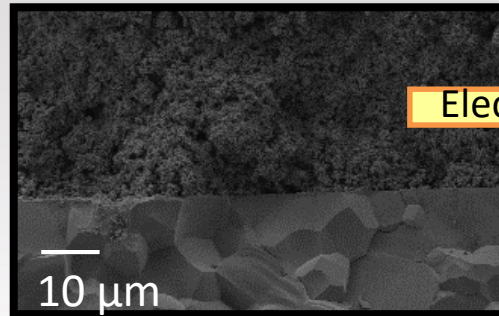
T = 700 °C

SEM micrographs of LSM/BCZY 60/40 % vol. infiltrated with Pr-Ce 50% (850 °C)

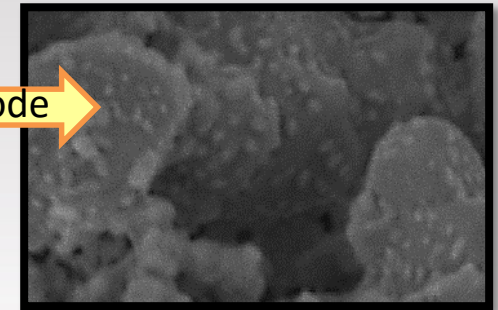
Powder 850 °C



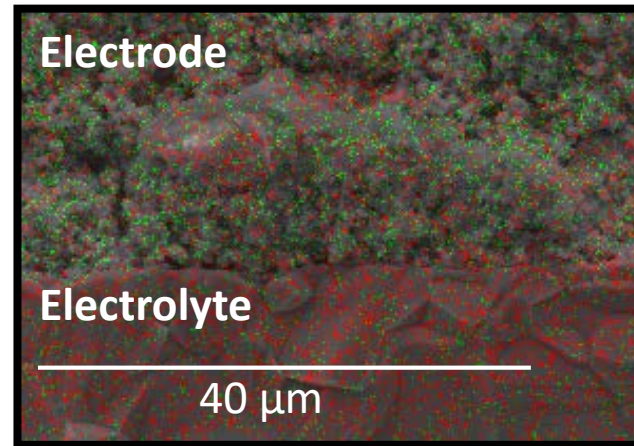
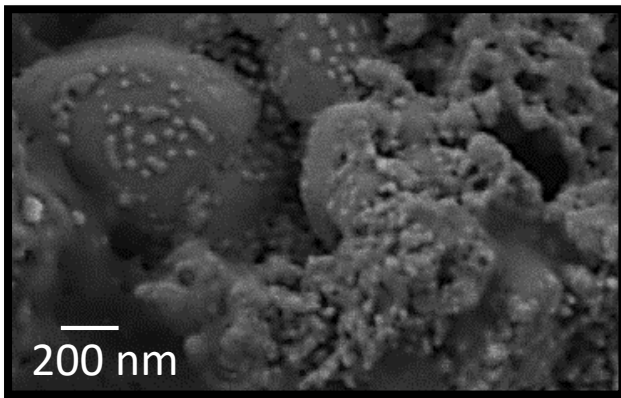
Fresh sample as a layer



Electrode



Electrode after operating conditions



- Ce
- Pr

Good infiltration

Multitube module



Multitube module

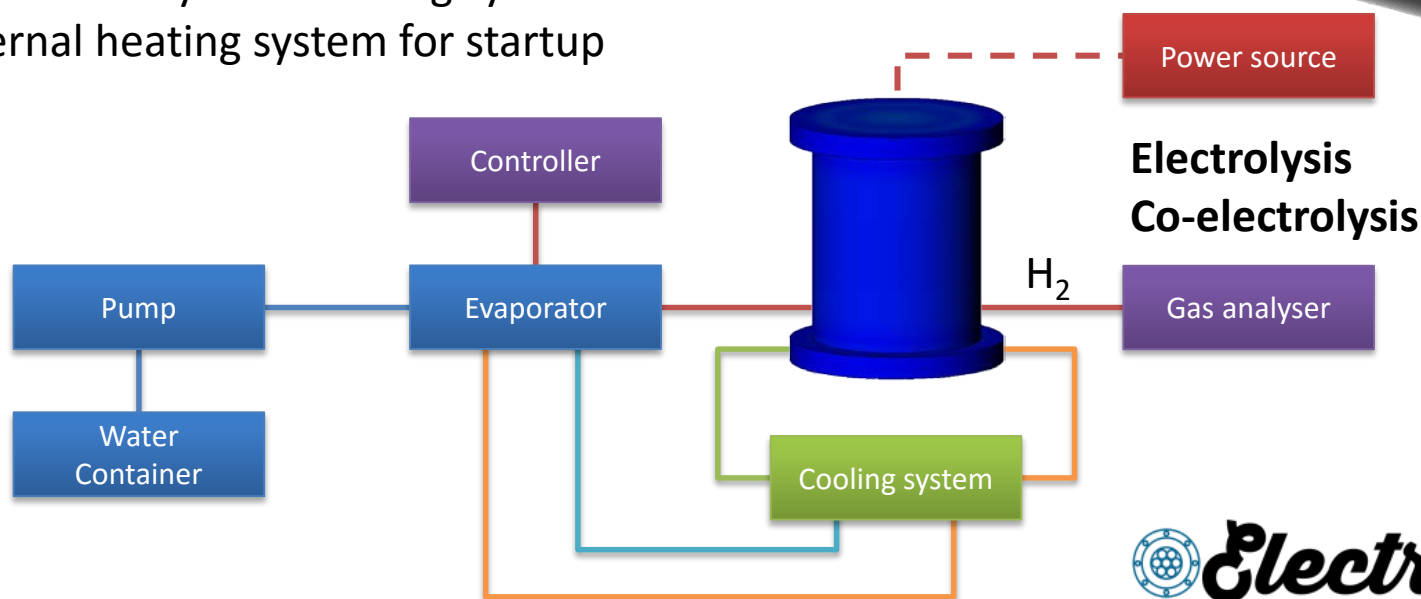
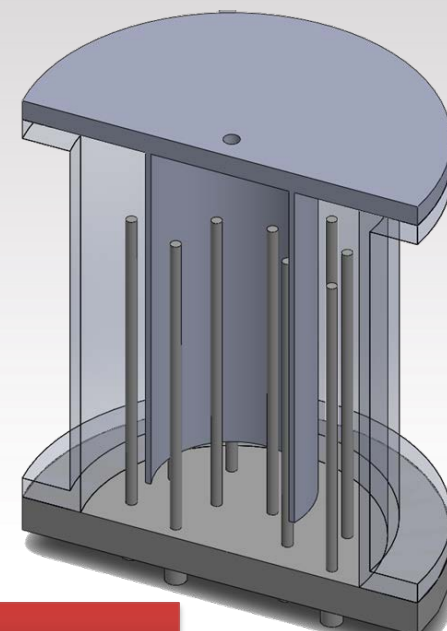
Multitube module achieves stable operation for H₂O electrolysis with H₂ production of 250 L_n/h using 1kW of power

Working conditions:

- Temperature: 700 °C
- Pressure:
 - ✓ Total: 50 bar
 - ✓ Steam: 10 bar
- Steam temperature: 250-300°C

Temperature management system:

- Cooling system allows applying low temperature gaskets
- Heat recovery from cooling system
- External heating system for startup



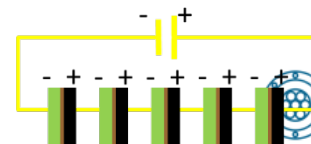
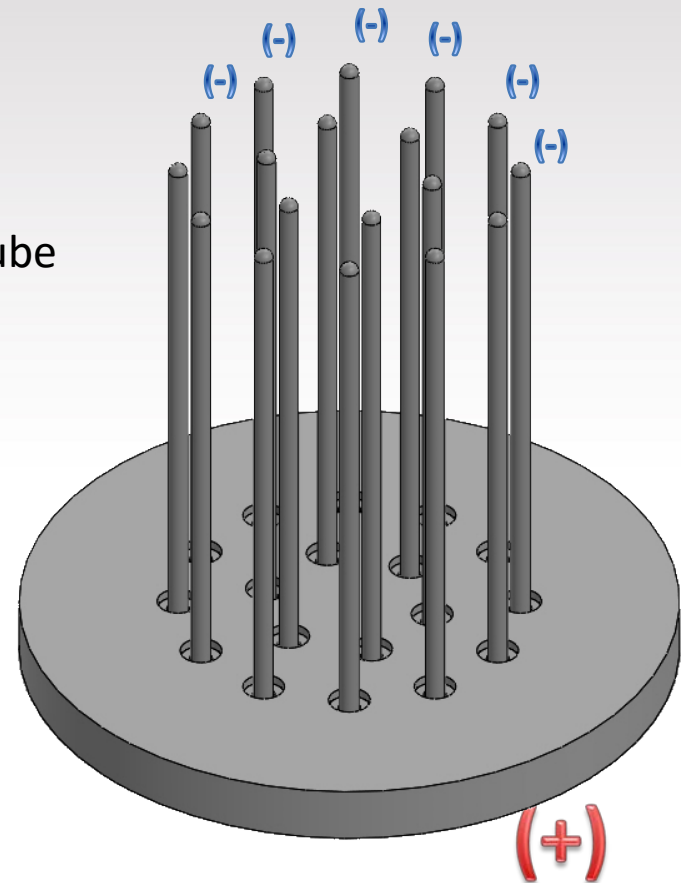
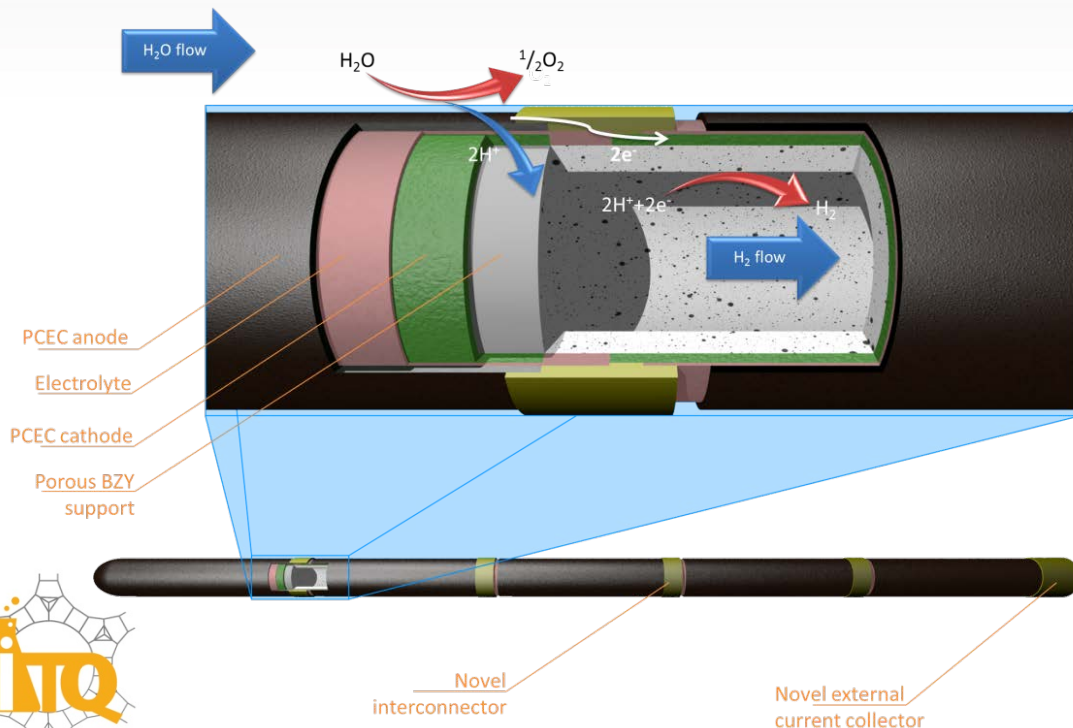
Multitube module

Tube materials

- Anode: LSM/BCZY or BGLC/BCZY (UiO)
- Cathode: Ni-BCZY cermet
- Electrolyte: BCZY

Electrical energy management system:

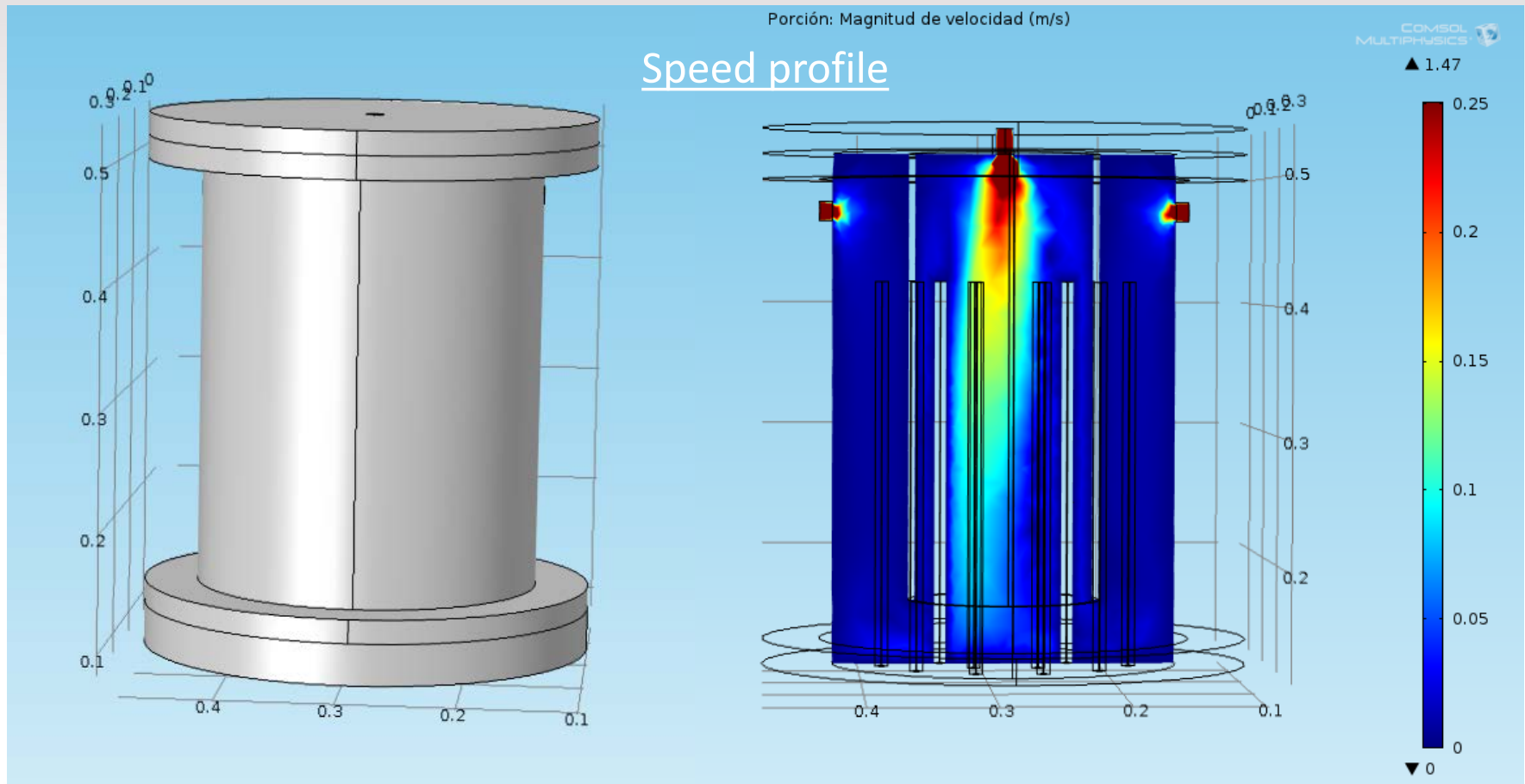
- Positive (+) current contact shared by all tubes
- Negative (-) current contacts independent for each tube
- One tube consists of 5 segments connected in series



Multitube module

Geometry optimisation:

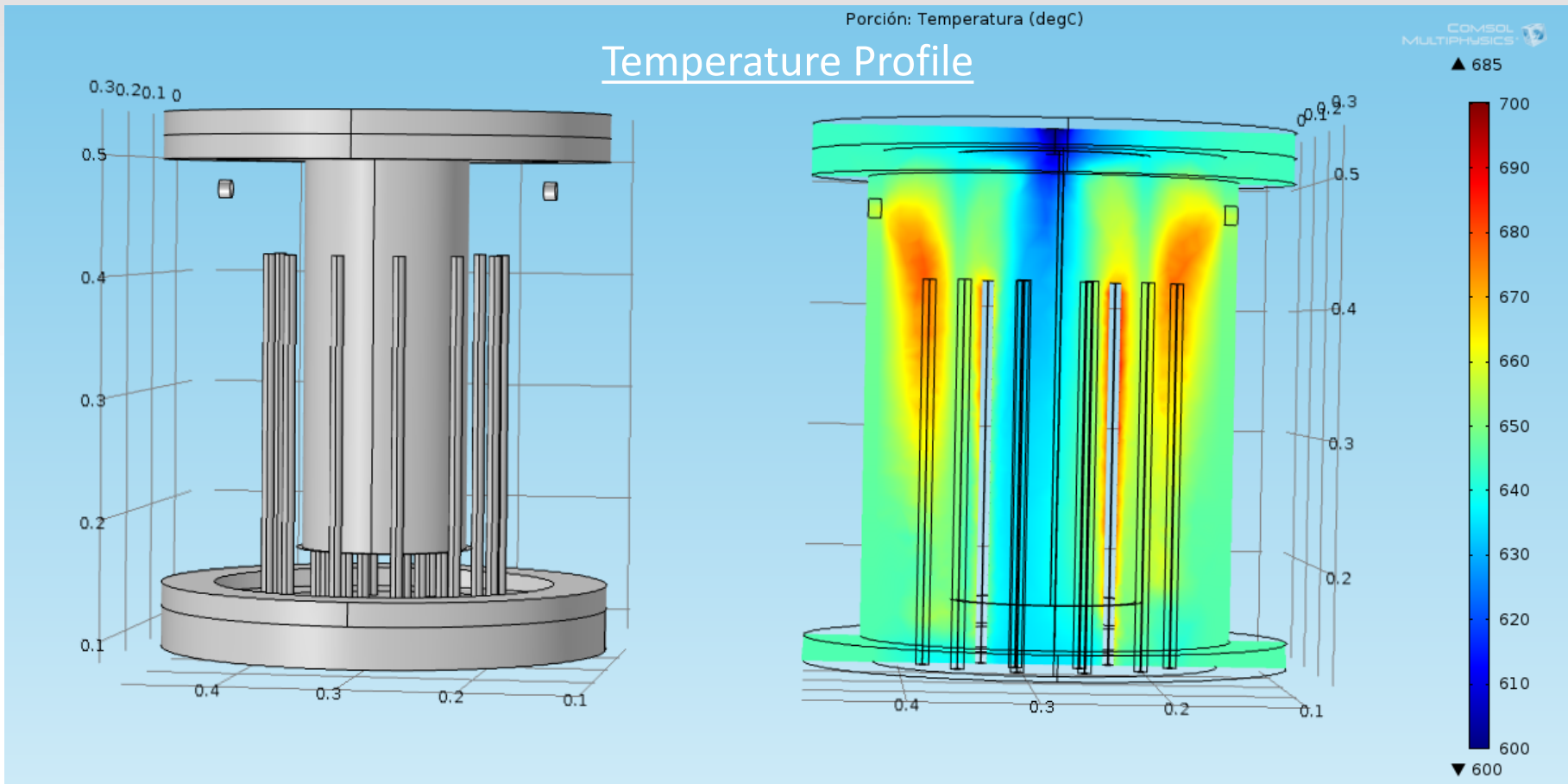
- Mechanical analysis (strength, thermal resistance)
- Fluid dynamics simulation (temperature profile and speed flow)



Multitube module

Geometry optimisation:

- Mechanical analysis (strength, thermal resistance)
- Fluid dynamics simulation (temperature profile and speed flow)

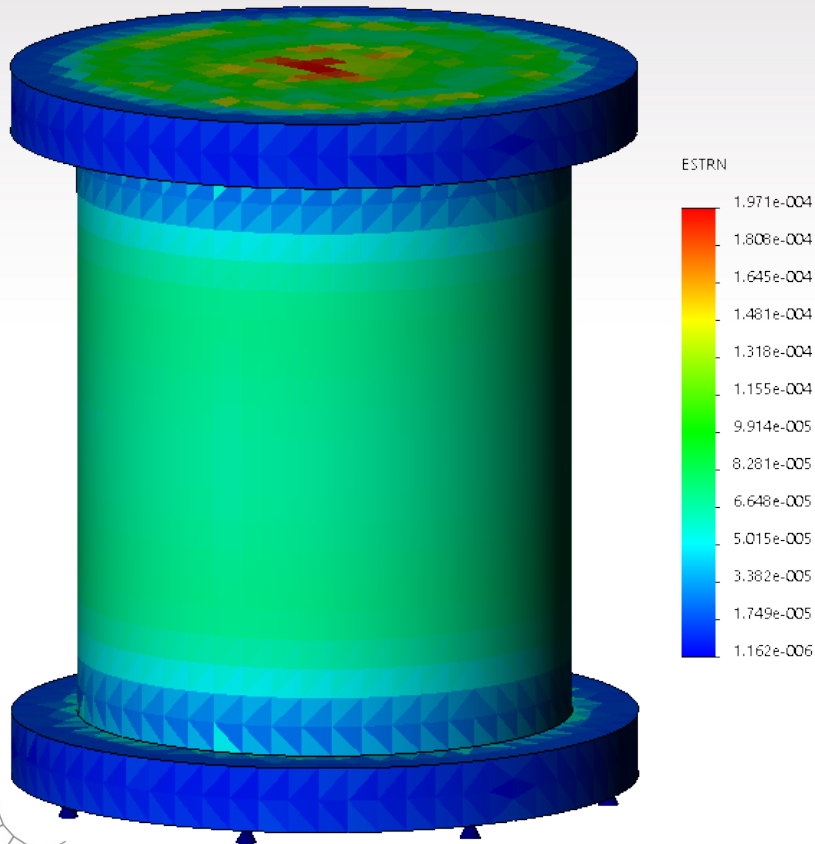


Multitube module

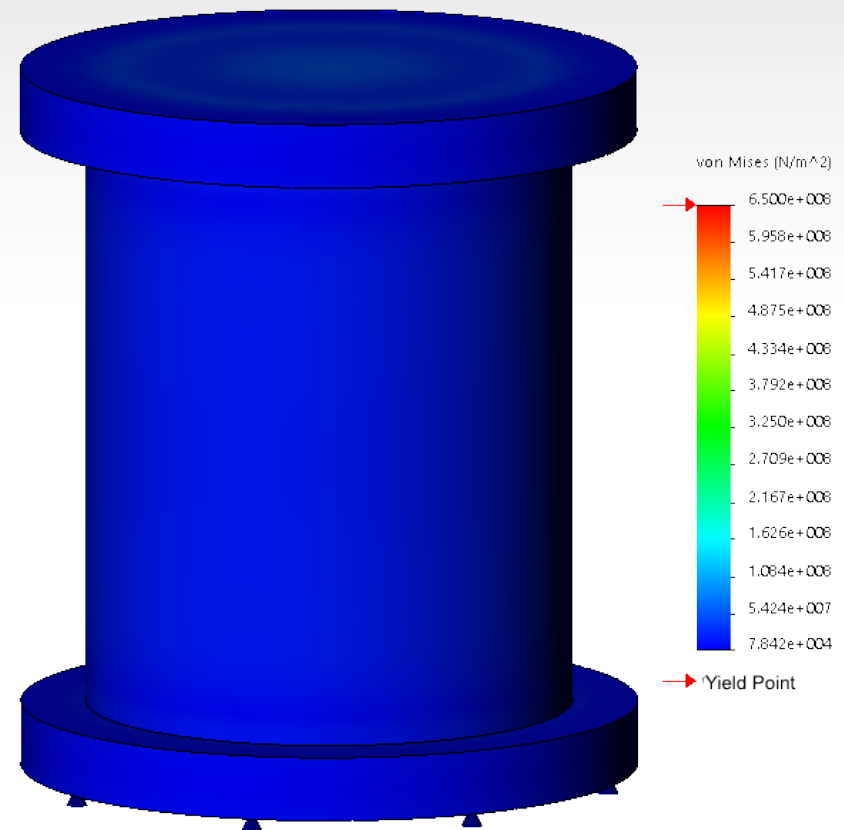
Geometry optimisation:

- Mechanical analysis (strength, thermal resistance)
- Fluid dynamics simulation (temperature profile and speed flow)

Displacement



Stress



Conclusions

- A thorough study by changing the measurement conditions (steam, pO_2 and total pressures)
- LSM/BCZY27 50/50 vol. % infiltrated with Pr shows the lower electrode R_p (700 °C)
- LSM/BCZY27 60/40 vol. % infiltrated with Pr-Ce and Ce show the lower electrode R_p when a current is applied (700 °C)
- Construction of a multitube module which allows efficient **electrolysis** of water and **co-electrolysis** of steam and CO_2 mixtures to obtain hydrocarbons

Acknowledgements

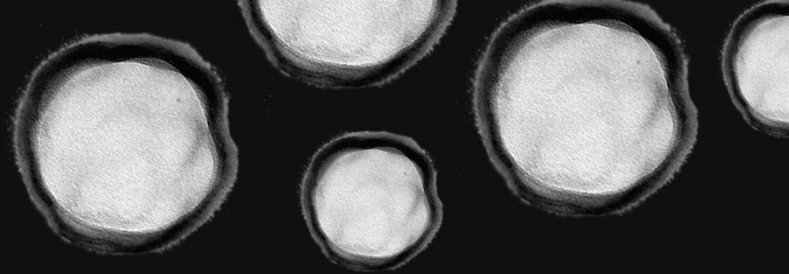
Financial support by the Spanish Government (Grants SEV-2012-0267 and MAT2011-29020-C02-01) and by the EU through FP7 Electra Project (Grant Agreement 621244)

My colleagues at ITQ/ELECTRA:





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Thank you for your attention



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